

# KINETIC THEORY OF GASES AND THERMODYNAMICS

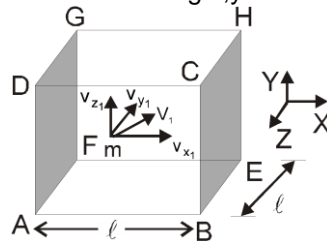
## KINETIC THEORY OF GASES:

Kinetic theory of gases is based on the following basic assumptions.

- A gas consists of very large number of molecules. These molecules are identical, perfectly elastic and hard spheres. They are so small that the volume of molecules is negligible as compared with the volume of the gas.
- Molecules do not have any preferred direction of motion, motion is completely random.
- These molecules travel in straight lines and in free motion most of the time. The time of the collision between any two molecules is very small.
- The collision between molecules and the wall of the container is perfectly elastic. It means kinetic energy is conserved in each collision.
- The path travelled by a molecule between two collisions is called free path and the mean of this distance travelled by a molecule is called mean free path.
- The motion of molecules is governed by Newton's law of motion
- The effect of gravity on the motion of molecules is negligible.

## EXPRESSION FOR THE PRESSURE OF A GAS:

Let us suppose that a gas is enclosed in a cubical box having length  $\ell$ . Let there are 'N' identical molecules, each having mass 'm'. Since the molecules are of same mass and perfectly elastic, so their mutual collisions result in the interchange of velocities only. Only collisions with the walls of the container contribute to the pressure by the gas molecules. Let us focus on a molecule having velocity  $v_1$  and components of velocity  $v_{x_1}, v_{y_1}, v_{z_1}$  along x, y and z-axis as shown in figure.



$$v_{12}^2 = v_{x_1}^2 + v_{y_1}^2 + v_{z_1}^2$$

The change in momentum of the molecule after one collision with wall BCHE

$$= m v_{x_1} - (-m v_{x_1}) = 2 m v_{x_1} .$$

The time taken between the successive impacts on the face BCHE =  $\frac{\text{distance}}{\text{velocity}} = \frac{2\ell}{v_{x_1}}$

Time rate of change of momentum due to collision =  $\frac{\text{change in momentum}}{\text{time taken}} = \frac{2mv_{x_1}}{2\ell / v_{x_1}} = \frac{mv_{x_1}^2}{\ell}$

Hence the net force on the wall BCHE due to the impact of n molecules of the gas is :

$$F_x = \frac{mv_{x_1}^2}{\ell} + \frac{mv_{x_2}^2}{\ell} + \frac{mv_{x_3}^2}{\ell} + \dots + \frac{mv_{x_n}^2}{\ell} = \frac{m}{\ell} (v_{x_1}^2 + v_{x_2}^2 + v_{x_3}^2 + \dots + v_{x_n}^2) = \frac{mN}{\ell} \langle v_x^2 \rangle$$

where  $\langle v_x^2 \rangle$  = mean square velocity in x-direction. Since molecules do not favour any particular direction therefore  $\langle v_x^2 \rangle = \langle v_y^2 \rangle = \langle v_z^2 \rangle$ . But  $\langle v^2 \rangle = \langle v_x^2 \rangle + \langle v_y^2 \rangle + \langle v_z^2 \rangle$

$$\Rightarrow \langle v_x^2 \rangle = \frac{\langle v^2 \rangle}{3} . \text{ Pressure is equal to force divided by area.}$$

$$P = \frac{F_x}{\ell^2} = \frac{M}{3\ell^3} \langle v^2 \rangle = \frac{M}{3V} \langle v^2 \rangle . \text{ Pressure is independent of x, y, z directions.}$$

Where  $\ell^3$  = volume of the container =  $V$

$M$  = total mass of the gas,  $\langle v^2 \rangle$  = mean square velocity of molecules

$$\Rightarrow P = \frac{1}{3} \rho \langle v^2 \rangle$$

As  $PV = nRT$ , then total translational K.E. of gas =  $\frac{1}{2} M \langle v^2 \rangle = \frac{3}{2} PV = \frac{3}{2} nRT$

Translational kinetic energy of 1 molecule =  $\frac{3}{2} kT$  (it is independent of nature of gas)

$$\langle v^2 \rangle = \frac{3P}{\rho} \quad \text{or} \quad v_{rms} = \sqrt{\frac{3P}{\rho}} = \sqrt{\frac{3RT}{M_{mole}}} = \sqrt{\frac{3kT}{m}}$$

Where  $v_{rms}$  is root mean square velocity of the gas.

Pressure exerted by the gas is  $P = \frac{1}{3} \rho \langle v^2 \rangle = \frac{2}{3} \times \frac{1}{2} \rho \langle v^2 \rangle$  or  $P = \frac{2}{3} E$ ,  $E = \frac{3}{2} P$

Thus total translational kinetic energy per unit volume (it is called energy density) of the gas is numerically

equal to  $\frac{3}{2}$  times the pressure exerted by the gas.

### IMPORTANT POINTS:

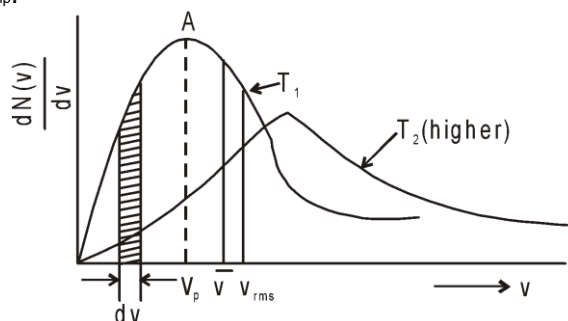
- $v_{rms} \propto \sqrt{T}$  and  $v_{rms} \propto \frac{1}{\sqrt{M_{mole}}}$
- At absolute zero, the motion of all molecules of the gas stops.
- At higher temperature and low pressure or at higher temperature and low density, a real gas behaves as an ideal gas.

### MAXWELL'S DISTRIBUTION LAW:

**Distribution Curve** – A plot of  $\frac{dN(v)}{dv}$  (number of molecules per unit speed interval) against  $c$  is known as Maxwell's distribution curve. The total area under the curve is given by the integral.

$$\int_0^{\infty} \frac{dN(v)}{dv} dv = \int_0^{\infty} dN(v) = N$$

Figure shows the distribution curves for two different temperatures. At any temperature the number of molecules in a given speed interval  $dv$  is given by the area under the curve in that interval (shown shaded). This number increases, as the speed increases, upto a maximum and then decreases asymptotically toward zero. Thus, maximum number of the molecules have speed lying within a small range centered about the speed corresponding the peak (A) of the curve. This speed is called the 'most probable speed'  $v_p$  or  $v_{mp}$ .



The distribution curve is asymmetrical about its peak (the most probable speed  $v_p$ ) because the lowest possible speed is zero, whereas there is no limit to the upper speed a molecule can attain. Therefore, the average speed  $\bar{v}$  is slightly larger than the most probable speed  $v_p$ . The root-mean-square speed,  $v_{rms}$ , is still larger ( $v_{rms} > \bar{v} > v_p$ ).

### Average (or Mean) Speed :

$$\bar{v} = \sqrt{\frac{8kT}{\pi m}} = 1.59 \sqrt{kT/m} \quad (\text{derivation is not in the course})$$

### RMS Speed :

$$v_{rms} = \sqrt{\langle v^2 \rangle} = \sqrt{\frac{3kT}{m}} = 1.73 \sqrt{\frac{kT}{m}}$$

### Most Probable Speed :

The most probable speed  $v_p$  or  $v_{mp}$  is the speed possessed by the maximum number of molecules, and corresponds to the maximum (peak) of the distribution curve. Mathematically, it is obtained by the condition.

$$\frac{dN(v)}{dv} = 0 \quad [\text{by substitution of formula of } dN(v) \text{ (which is not in the course)}]$$

Hence the most probable speed is

$$v_p = \sqrt{\frac{2kT}{m}} = 1.41 \sqrt{kT/m}$$

From the above expression, we can see that

$$v_{rms} > \bar{v} > v_p$$

## DEGREE OF FREEDOM:

Total number of independent co-ordinates which must be known to completely specify the position and configuration of dynamical system is known as "degree of freedom  $f$ ". Maximum possible translational

$$\left( \frac{1}{2} m v_x^2 + \frac{1}{2} m v_y^2 + \frac{1}{2} m v_z^2 \right)$$

degrees of freedom are three i.e.

$$\left( \frac{1}{2} I_x \omega_x^2 + \frac{1}{2} I_y \omega_y^2 + \frac{1}{2} I_z \omega_z^2 \right)$$

Maximum possible rotational degrees of freedom are three i.e.

Vibrational degrees of freedom are two i.e. (Kinetic energy of vibration and Potential energy of vibration)

**Mono atomic :** (all inert gases, He, Ar etc.)  $f = 3$  (translational)

**Diatomic :** (gases like  $H_2$ ,  $N_2$ ,  $O_2$  etc.)  $f = 5$  (3 translational + 2 rotational)

If temp  $< 70$  K for diatomic molecules, then  $f = 3$

If temp in between 250 K to 5000 K, then  $f = 5$

If temp  $> 5000$  K  $f = 7$  [ 3 translational + 2 rotational + 2 vibrational ]

## MAXWELL'S LAW OF EQUIPARTITION OF ENERGY:

Energy associated with each degree of freedom =  $\frac{1}{2} kT$ . If degree of freedom of a molecule is  $f$ , then

$$U = \frac{1}{2} f k T$$

total kinetic energy of that molecule

### INTERNAL ENERGY:

The internal energy of a system is the sum of kinetic and potential energies of the molecules of the system. It is denoted by  $U$ . Internal energy ( $U$ ) of the system is the function of its absolute temperature ( $T$ ) and its volume ( $V$ ). i.e.  $U = f(T, V)$

In case of an ideal gas, intermolecular force is zero. Hence its potential energy is also zero. In this case, the internal energy is only due to kinetic energy, which depends on the absolute temperature of the gas.

$$\text{i.e. } U = f(T). \text{ For an ideal gas internal energy } U = \frac{f}{2} nRT.$$

## Solved Examples

**Example 1.** A light container having a diatomic gas enclosed with in is moving with velocity  $v$ . Mass of the gas is  $M$  and number of moles is  $n$ .

- What is the kinetic energy of gas w.r.t. centre of mass of the system?
- What is K.E. of gas w.r.t. ground?

**Solution :**

mass of gas =  $M$   
 temperature  $T$

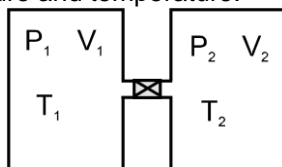
$\rightarrow v$

(i) K.E. =  $\frac{5}{2} nRT$

(ii) Kinetic energy of gas w.r.t. ground = Kinetic energy of centre of mass w.r.t. ground + Kinetic energy of gas w.r.t. centre of mass.

$$\text{K.E.} = \frac{1}{2} MV^2 + \frac{5}{2} nRT$$

**Example 2.** Two nonconducting containers having volume  $V_1$  and  $V_2$  contain monoatomic and diatomic gases respectively. They are connected as shown in figure. Pressure and temperature in the two containers are  $P_1, T_1$  and  $P_2, T_2$  respectively. Initially stop cock is closed, if the stop cock is opened find the final pressure and temperature.



**Solution :**

$$n_1 = \frac{P_1 V_1}{RT_1} \quad n_2 = \frac{P_2 V_2}{RT_2}$$

$n = n_1 + n_2$  (number of moles are conserved)

Finally pressure in both parts & temperature of the both the gases will be become equal.

$$\frac{P(V_1 + V_2)}{RT} = \frac{P_1 V_1}{RT_1} + \frac{P_2 V_2}{RT_2}$$

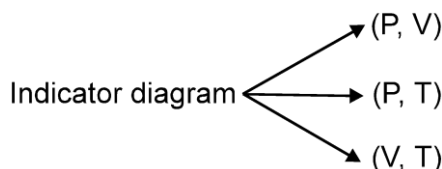
From energy conservation

$$\frac{3}{2} n_1 RT_1 + \frac{5}{2} n_2 RT_2 = \frac{3}{2} n RT + \frac{5}{2} n RT$$

$$\Rightarrow T = \frac{(3P_1 V_1 + 5P_2 V_2) T_1 T_2}{3P_1 V_1 T_2 + 5P_2 V_2 T_1} \Rightarrow P = \left( \frac{3P_1 V_1 + 5P_2 V_2}{3P_1 V_1 T_2 + 5P_2 V_2 T_1} \right) \left( \frac{P_1 V_1 T_2 + P_2 V_2 T_2}{V_1 + V_2} \right)$$

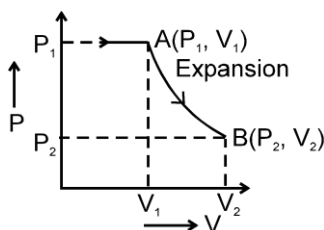

## INDICATOR DIAGRAM:

A graph representing the variation of pressure or variation of temperature or variation of volume with each other is called or indicator diagram.



(A) Every point of Indicator diagram represents a unique state ( $P, V, T$ ) of gases.

(B) Every curve on Indicator diagram represents a unique process.



## THERMODYNAMICS

Thermodynamics is mainly the study of exchange of heat energy between bodies and conversion of the same into mechanical energy and vice versa.

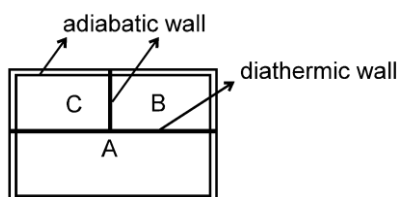
## THERMODYNAMIC SYSTEM

Collection of an extremely large number of atoms or molecules confined within certain boundaries such that it has a certain value of pressure (P), volume (V) and temperature (T) is called a **thermodynamic system**. Anything outside the thermodynamic system to which energy or matter is exchanged is called its surroundings. Taking into consideration the interaction between a system and its surroundings thermodynamic system is divided into three classes :

- Open system** : A system is said to be an open system if it can exchange both energy and matter with its surroundings.
- Closed system** : A system is said to be closed system if it can exchange only energy (not matter with its surroundings).
- Isolated system** : A system is said to be isolated if it can neither exchange nor matter with its surroundings.

## ZEROTH LAW OF THERMODYNAMICS:

If two systems (B and C) are separately in thermal equilibrium with a third one (A), then they themselves are in thermal equilibrium with each other.



## EQUATION OF STATE (FOR IDEAL GASES):

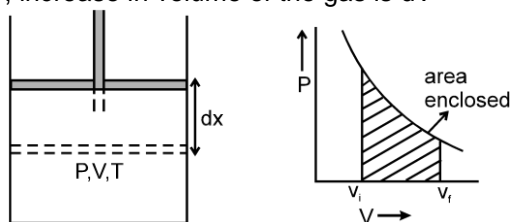
The relation between the thermodynamic variables (P, V, T) of the system is called equation of state. The equation of state for an ideal gas of n moles is given by  $PV = nRT$ ,

## WORK DONE BY A GAS:

Let P and V be the pressure and volume of the gas. If A be the area of the piston, then force exerted by gas on the piston is,  $F = P \times A$ .

Let the piston move through a small distance dx during the expansion of the gas. Work done for a small displacement dx is  $dW = F dx = PA dx$

Since  $A dx = dV$ , increase in volume of the gas is  $dV \Rightarrow dW = P dV$



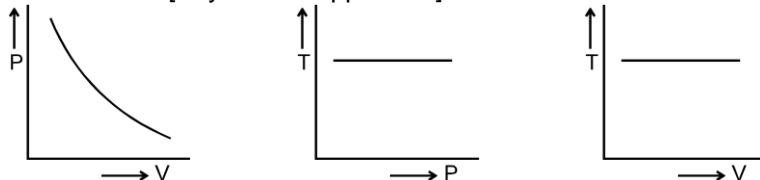
$$\text{or } W = \int dW = \int P dV$$

Area enclosed under P-V curve gives work done during process.

## DIFFERENT TYPES OF PROCESSES:

- Isothermal Process** :

$T = \text{constant}$  [Boyle's law applicable]  $PV = \text{constant}$



## Kinetic Theory of Gases & Thermodynamics

There is exchange of heat between system and surroundings. System should be compressed or expanded

very slowly so that there is sufficient time for exchange of heat to keep the temperature constant.

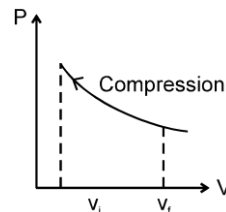
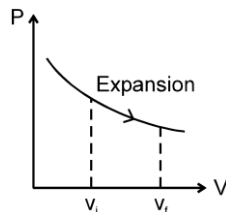
**Slope of P-V curve in isothermal process:**

$$PV = \text{constant} = C \Rightarrow \frac{dP}{dV} = -\frac{P}{V}$$

**Work done in isothermal process:**

$$W = nRT \ln \frac{V_f}{V_i} \quad \left[ \begin{array}{l} \text{If } v_f > v_i \text{ then } W \text{ is positive} \\ \text{If } v_f < v_i \text{ then } W \text{ is negative} \end{array} \right]$$

$$W = \left[ 2.303 nRT \log_{10} \frac{V_f}{V_i} \right]$$



**Internal energy in isothermal process :**

$$U = f(T) \Rightarrow \Delta U = 0$$

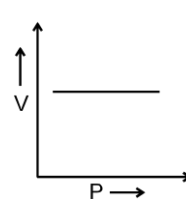
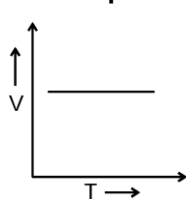
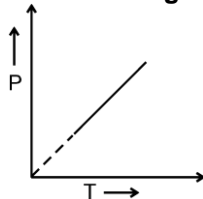
**(b) Iso- Choric Process (Isometric Process) :**

$$\begin{aligned} &\Rightarrow V = \text{constant} \\ &\Rightarrow \text{change in volume is zero} \\ &\Rightarrow \frac{P}{T} \text{ is constant} \\ &\Rightarrow \frac{P}{T} = \text{const.} \quad (\text{Galussac-law}) \end{aligned}$$

**Work done in isochoric process :**

$$\text{Since change in volume is zero therefore } dW = p \, dV = 0$$

**Indicator diagram of isochoric process :**



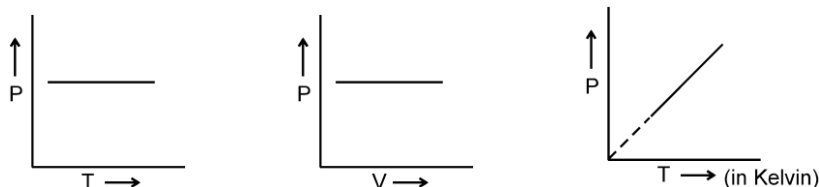
$$\text{Change in internal energy in isochoric process : } \Delta U = n \frac{f}{2} R \Delta T$$

$$\text{Heat given in isochoric process : } \Delta Q = \Delta U = n \frac{f}{2} R \Delta T$$

**(c) Isobaric Process :** Pressure remains constant in isobaric process

$$\therefore P = \text{constant} \Rightarrow \frac{V}{T} = \text{constant}$$

**Indicator diagram of isobaric process :**



**Work done in isobaric process :**

$$\Delta W = P \Delta V = P (V_{\text{final}} - V_{\text{initial}}) = nR (T_{\text{final}} - T_{\text{initial}})$$

**Change in internal energy in isobaric process :**  $\Delta U = n C_v \Delta T$

**Heat given in isobaric process :**

$$\Delta Q = \Delta U + \Delta W$$

$$\Delta Q = n \frac{f}{2} R \Delta T + P [V_f - V_i] = n \frac{f}{2} R \Delta T + nR \Delta T$$

Above expression gives an idea that to increase temperature by  $\Delta T$  in isobaric process heat required is more than in isochoric process.

(d) **Cyclic Process :** In the cyclic process initial and final states are same therefore initial state = final state

Work done = Area enclosed under P-V diagram.

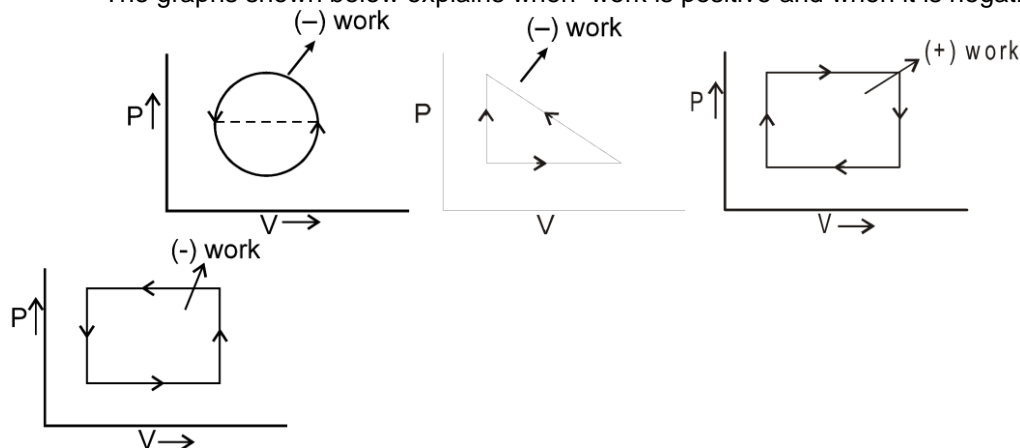
Change in internal Energy  $\Delta U = 0$

$$\Delta Q = \Delta U + \Delta W$$

$$\therefore \Delta Q = \Delta W$$

If the process on P-V curve is clockwise, then net work done is (+ve) and vice-versa.

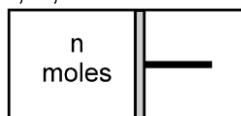
The graphs shown below explains when work is positive and when it is negative



## Solved Examples

**Example 3.**

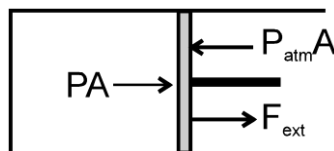
The cylinder shown in the figure has conducting walls and temperature of the surrounding is  $T$ , the piston is initially in equilibrium, the cylinder contains  $n$  moles of a gas. Now the piston is displaced slowly by an external agent to make the volume double of the initial. Find work done by external agent in terms of  $n$ ,  $R$ ,  $T$



**Solution :**

**1st Method :**

Work done by external agent is positive, because  $F_{\text{ext}}$  and displacement are in the same direction. Since walls are conducting therefore temperature remains constant.



Applying equilibrium condition when pressure of the gas is P

$$PA + F_{\text{ext}} = P_{\text{atm}} A$$

$$F_{\text{ext}} = P_{\text{atm}} A - PA$$

$$\begin{aligned} W_{\text{ext}} &= \int_0^d F_{\text{ext}} dx = \int_0^d P_{\text{atm}} A dx - \int_0^d PA dx \\ &= P_{\text{atm}} A \int_0^d dx - \int_{V_0}^{2V_0} \frac{nRT}{V} dV \\ &= P_{\text{atm}} A d - nRT \ln 2 \\ &= P_{\text{atm}} \cdot V_0 - nRT \ln 2 = nRT (1 - \ln 2) \end{aligned}$$

## 2nd Method

Applying work energy theorem on the piston

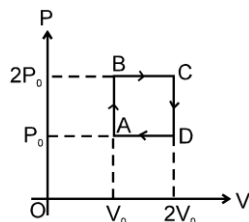
$$\Delta k = 0$$

$$W_{\text{all}} = \Delta k$$

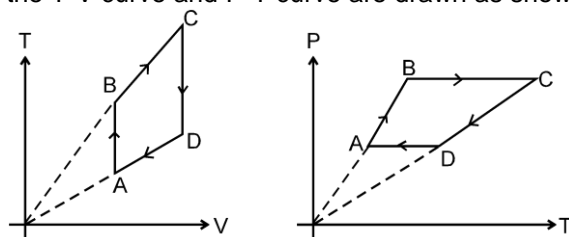
$$W_{\text{gas}} + W_{\text{atm}} + W_{\text{ext}} = 0$$

$$\begin{aligned} nRT \ln \frac{V_f}{V_i} - nRT + W_{\text{ext}} &= 0 \\ W_{\text{ext}} &= nRT (1 - \ln 2) \end{aligned}$$

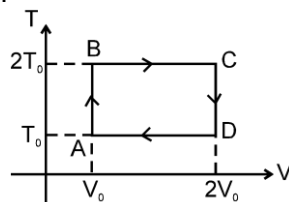
**Example 4.** Find out the work done in the given graph. Also draw the corresponding T-V curve and P-T curve.



**Solution :** Since in P-V curves area under the cycle is equal to work done therefore work done by the gas is equal to  $P_0 V_0$ . Line AB and CD are isochoric line, line BC and DA are isobaric line.  
 $\therefore$  the T-V curve and P-T curve are drawn as shown.



**Example 5.** T-V curve of cyclic process is shown below, number of moles of the gas are n find the total work done during the cycle.



**Solution :** Since path AB and CD are isochoric therefore work done is zero during path AB and CD. Process BC and DA are isothermal, therefore

$$W_{BC} = nR2T_0 \ln \frac{V_C}{V_B} = 2nRT_0 \ln 2$$

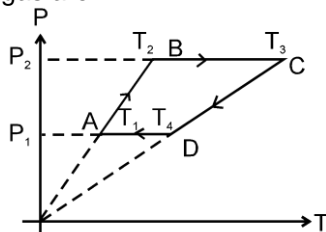


$$W_{DA} = nRT_0 \ln \frac{V_A}{V_D} = -nRT_0 \ln 2$$

$$\text{Total work done} = W_{BC} + W_{DA} = 2nRT_0 \ln 2 - nRT_0 \ln 2$$

$$= nRT_0 \ln 2$$

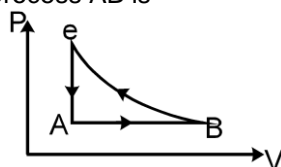
**Example 6.** P-T curve of a cyclic process is shown. Find out the work done by the gas in the given process if number of moles of the gas are n.



**Solution :** Since path AB and CD are isochoric therefore work done during AB and CD is zero. Path BC and DA are isobaric.  
Hence  $W_{BC} = nR\Delta T = nR(T_3 - T_2)$   
 $W_{DA} = nR(T_1 - T_4)$   
Total work done  $= W_{BC} + W_{DA} = nR(T_1 + T_3 - T_4 - T_2)$

**Example 7.** Consider the cyclic process ABCA on a sample of 2.0 mol of an ideal gas as shown in figure. The temperatures of the gas at A and B are 300 K and 500 K respectively. A total of 1200 J heat is withdrawn from the sample in the process. Find the work done by the gas in part BC. Take  $R = 8.3 \text{ J/mol-K}$ .

**Solution :** The change in internal energy during the cyclic process is zero. Hence, the heat supplied to the gas is equal to the work done by it. Hence,  
 $W_{AB} + W_{BC} + W_{CA} = -1200 \text{ J.}$  .....(i)  
The work done during the process AB is



$$W_{AB} = P_A (V_B - V_A)$$

$$= nR(T_B - T_A)$$

$$= (2.0 \text{ mol}) (8.3 \text{ J/mol-K}) (200 \text{ K})$$

$$= 3320 \text{ J}$$

The work done by the gas during the process CA is zero as the volume remains constant. From (i),

$$3320 \text{ J} + W_{BC} = -1200 \text{ J}$$

$$\text{or } W_{BC} = -4520 \text{ J.}$$

$$= -4520 \text{ J.}$$



## FIRST LAW OF THERMODYNAMICS:

The first law of thermodynamics is the law of conservation of energy. It states that if a system absorbs heat  $dQ$  and as a result the internal energy of the system changes by  $dU$  and the system does a work  $dW$ , then  $dQ = dU + dW$ .

But,  $dW = P dV$   $dQ = dU + P dV$

which is the mathematical statement of first law of thermodynamics.

**Heat gained by a system, work done by a system and increase in internal energy are taken as positive.**

**Heat lost by a system, work done on a system and decrease in internal energy are taken as negative.**

## Solved Examples

## Kinetic Theory of Gases & Thermodynamics

**Example 8.** 1 gm water at 100°C is heated to convert into steam at 100°C at 1 atm. Find out change in internal energy of water. It is given that volume of 1 gm water at 100°C = 1 cc. volume of 1 gm steam at 100°C = 1671 cc. Latent heat of vaporization = 540 cal/g. (Mechanical equivalent of heat J = 4.2J/cal.)

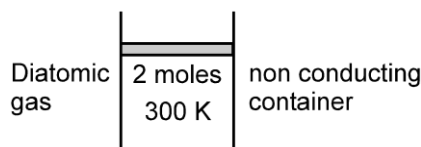
**Solution :** From first law of thermodynamic  $\Delta Q = \Delta u + \Delta w$

$$\Delta Q = mL = 1 \times 540 \text{ cal.} = 540 \text{ cal.}$$

$$\Delta W = P\Delta V = \frac{10^5(1671-1) \times 10^{-6}}{4.2} = \frac{10^5 \times 1670 \times 10^{-6}}{4.2} = 40 \text{ cal.}$$

$$\Delta u = 540 - 40 = 500 \text{ cal.}$$

**Example 9.** Two moles of a diatomic gas at 300 K are kept in a non-conducting container enclosed by a piston. Gas is now compressed to increase the temperature from 300 K to 400 K. Find work done by the gas



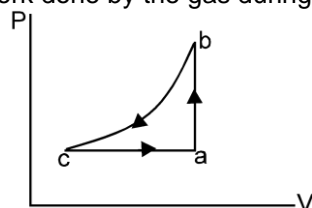
**Solution :**  $\Delta Q = \Delta u + \Delta w$

Since container is non-conducting therefore

$$\Delta Q = 0 = \Delta u + \Delta w$$

$$\Rightarrow \Delta W = -\Delta u = -n \frac{f}{2} R \Delta T = -2 \times \frac{5}{2} R (400 - 300) \\ = -5 \times 8.314 \times 100 \text{ J} = -5 \times 831.4 \text{ J} = -4157 \text{ J}$$

**Example 10.** A sample of an ideal gas is taken through the cyclic process abca (figure). It absorbs 50 J of heat during the part ab, no heat during bc and rejects 70 J of heat during ca. 40 J of work is done on the gas during the part bc. (a) Find the internal energy of the gas at b and c if it is 1500 J at a. (b) Calculate the work done by the gas during the part ca.



**Solution :** (a) In the part ab the volume remains constant. Thus, the work done by the gas is zero. The heat absorbed by the gas is 50 J. The increase in internal energy from a to b is

$$\Delta U = \Delta Q = 50 \text{ J.}$$

As the internal energy is 1500 J at a, it will be 1550 J at b. In the part bc, the work done by the gas is  $\Delta W = -40 \text{ J}$  and no heat is given to the system. The increase in internal energy from b to c is

$$\Delta U = -\Delta W = 40 \text{ J.}$$

As the internal energy is 1550 J at b, it will be 1590 J at c.

(b) The change in internal energy from c to a is

$$\Delta U = 1500 \text{ J} - 1590 \text{ J} = -90 \text{ J.}$$

The heat given to the system is  $\Delta Q = -70 \text{ J}$ .

Using  $\Delta Q = \Delta U + \Delta W$ ,

$$\Delta W_{ca} = \Delta Q - \Delta U \\ = -70 \text{ J} + 90 \text{ J} = 20 \text{ J.}$$

**Example 11.** The internal energy of a monatomic ideal gas is  $1.5 nRT$ . One mole of helium is kept in a cylinder of cross-section  $8.5 \text{ cm}^2$ . The cylinder is closed by a light frictionless piston. The gas is heated slowly in a process during which a total of 42 J heat is given to the gas. If the temperature rises through  $2^\circ\text{C}$ , find the distance moved by the piston. Atmospheric pressure = 100 kPa.

## Kinetic Theory of Gases & Thermodynamics

**Solution :** The change in internal energy of the gas is  

$$\Delta U = 1.5 nR (\Delta T)$$

$$= 1.5 (1 \text{ mol}) (8.3 \text{ J/mol-K}) (2\text{K})$$

$$= 24.9 \text{ J.}$$

The heat given to the gas = 42 J

The work done by the gas is

$$\Delta W = \Delta Q - \Delta U$$

$$= 42 \text{ J} - 24.9 \text{ J} = 17.1 \text{ J.}$$

If the distance moved by the piston is  $x$ , the work done is

$$\Delta W = (100 \text{ kPa}) (8.5 \text{ cm}^2) x.$$

Thus,  $(10^5 \text{ N/m}^2) (8.5 \times 10^{-4} \text{ m}^2) x = 17.1 \text{ J}$

or,  $x = 0.2 \text{ m} = 20 \text{ cm.}$

**Example 12.** A sample of ideal gas ( $f = 5$ ) is heated at constant pressure. If an amount 140 J of heat is supplied to the gas, find (a) the change in internal energy of the gas (b) the work done by the gas.

**Solution :** Suppose the sample contains  $n$  moles. Also suppose the volume changes from  $V_1$  to  $V_2$  and the temperature changes from  $T_1$  to  $T_2$ .

The heat supplied is

$$\Delta Q = \Delta U + P\Delta V = \Delta U + nR\Delta T = \Delta U + \frac{2\Delta U}{f}$$

(a) The change in internal energy is

$$\Delta U = n \frac{f}{2} R (T_2 - T_1) = n \frac{f}{2} R (T_2 - T_1)$$

$$= \frac{f}{2+f} \Delta Q = \frac{140 \text{ J}}{1.4} = 100 \text{ J.}$$

(b) The work done by the gas is

$$\Delta W = \Delta Q - \Delta U$$

$$= 140 \text{ J} - 100 \text{ J} = 40 \text{ J.}$$



### Efficiency of a cycle ( $\eta$ ) :

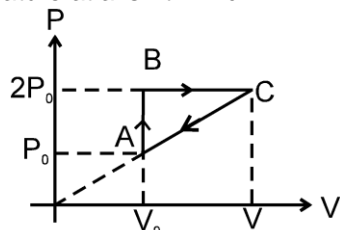
$$\eta = \frac{\text{total Mechanical work done by the gas in the whole process}}{\text{Heat absorbed by the gas (only +ve)}}$$

$$= \frac{\text{area under the cycle in P-V curve}}{\text{Heat injected into the system}}$$

$$\eta = \left(1 - \frac{Q_2}{Q_1}\right) \quad \text{for Heat Engine,} \quad \eta = \left(1 - \frac{T_2}{T_1}\right) \quad \text{for Carnot cycle}$$

### Solved Examples

**Example 13.**  $n$  moles of a diatomic gas has undergone a cyclic process ABC as shown in figure. Temperature at a is  $T_0$ . Find



- Volume at C ?
- Maximum temperature ?
- Total heat given to gas ?
- Is heat rejected by the gas, if yes how much heat is rejected ?
- Find out the efficiency

**Solution :**

- (i) Since triangle O A V<sub>0</sub> and OC V are similar therefore

$$\frac{2P_0}{V} = \frac{P_0}{V_0} \Rightarrow V = 2V_0$$

- (ii) Since process AB is isochoric hence

$$\frac{P_A}{T_A} = \frac{P_B}{T_B} \Rightarrow T_B = 2T_0$$

Since process BC is isobaric therefore  $\frac{T_B}{V_B} = \frac{T_C}{V_C}$   
 $\Rightarrow T_C = 2T_B = 4T_0$

- (iii) Since process is cyclic therefore

$$\Delta Q = \Delta W = \text{area under the cycle} = \frac{1}{2} P_0 V_0$$

- (iv) Since  $\Delta u$  and  $\Delta W$  both are negative in process CA

$\therefore \Delta Q$  is negative in process CA and heat is rejected in process CA

$$\Delta Q_{CA} = \Delta W_{CA} + \Delta U_{CA}$$

$$\begin{aligned} &= -\frac{1}{2} [P_0 + 2P_0] V_0 - \frac{5}{2} nR (T_c - T_a) \\ &= -\frac{1}{2} [P_0 + 2P_0] V_0 - \frac{5}{2} nR \left( \frac{4P_0 V_0}{nR} - \frac{P_0 V_0}{nR} \right) \\ &= -9P_0 V_0 = \text{Heat injected.} \end{aligned}$$

(v)  $\eta = \text{efficiency of the cycle} = \frac{\text{work done by the gas}}{\text{heat injected}} = \eta = \frac{P_0 V_0 / 2}{Q_{\text{injected}}} \times 100$

$$\Delta Q_{\text{inj}} = \Delta Q_{AB} + \Delta Q_{BC}$$

$$\begin{aligned} &= \left[ \frac{5}{2} nR(2T_0 - T_0) \right] + \left[ \frac{5}{2} nR(2T_0) + 2P_0(2V_0 - V_0) \right] = \frac{19}{2} P_0 V_0 \\ \eta &= \frac{100}{19} \% \end{aligned}$$



## SPECIFIC HEAT :

The specific heat capacity of a substance is defined as the heat supplied per unit mass of the substance per unit rise in the temperature. If an amount  $\Delta Q$  of heat is given to a mass  $m$  of the substance and its temperature rises by  $\Delta T$ , the specific heat capacity  $s$  is given by equation

$$s = \frac{\Delta Q}{m \Delta T}$$

The molar heat capacities of a gas are defined as the heat given per mole of the gas per unit rise in the temperature. The molar heat capacity at constant volume, denoted by  $C_v$ , is :

$$C_v = \left( \frac{\Delta Q}{n \Delta T} \right)_{\text{constant volume}} = \frac{f}{2} R$$

and the molar heat capacity at constant pressure, denoted by  $C_p$  is,

$$C_p = \left( \frac{\Delta Q}{n \Delta T} \right)_{\text{constant volume}} = \left( \frac{f}{2} + 1 \right) R$$

where  $n$  is the amount of the gas in number of moles and  $f$  is degree of freedom. Quite often, the term specific heat capacity or specific heat is used for molar heat capacity. It is advised that the unit be carefully noted to determine the actual meaning. The unit of specific heat capacity is J/kg-K whereas that of molar heat capacity is J/mol-K.

## MOLAR HEAT CAPACITY OF IDEAL GAS IN TERMS OF R :

- (i) For a monoatomic gas  $f = 3$

$$C_V = \frac{3}{2} R, \quad C_P = \frac{5}{2} R$$

$$\Rightarrow \frac{C_P}{C_V} = \gamma = \frac{5}{3} = 1.67$$

(ii) For a diatomic gas  $f = 5$

$$C_V = \frac{5}{2} R, \quad C_P = \frac{7}{2} R$$

$$\gamma = \frac{C_P}{C_V} = 1.4$$

(iii) For a Triatomic gas  $f = 6$

$$C_V = 3R, \quad C_P = 4R$$

$$\gamma = \frac{C_P}{C_V} = \frac{4}{3} = 1.33$$

[Note for  $\text{CO}_2$ ;  $f = 5$ , it is linear]

In general if  $f$  is the degree of freedom of a molecule, then,

$$C_V = \frac{f}{2} R, \quad C_P = \left(\frac{f}{2} + 1\right) R, \quad \gamma = \frac{C_P}{C_V} = \left[1 + \frac{2}{f}\right]$$

## Solved Examples

**Example 14** In a thermodynamic process, the pressure of a certain mass of gas is changed in such a way that 20 Joule heat is released from it and 8 Joule work is done on the gas. If the initial internal energy of the system is 30 joule then the final internal energy will be -

**Solution.**  $dQ = dU + dW \Rightarrow dQ = U_{\text{final}} - U_{\text{initial}} + dW$   
 $U_{\text{final}} = dQ - dW + U_{\text{initial}}$  or  $U_{\text{final}} = -20 + 8 + 30$  of  $U_{\text{final}} = 18 \text{ Joule}$

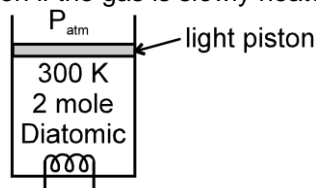
**Example 15** A gas is contained in a vessel fitted with a movable piston. The container is placed on a hot stove. A total of 100 cal of heat is given to the gas & the gas does 40 J of work in the expansion resulting from heating. Calculate the increase in internal energy in the process.

**Solution.** Heat given to the gas is  $\Delta Q = 100 \text{ cal} = 418 \text{ J}$ .  
 Work done by the gas is  $\Delta W = 40 \text{ J}$   
 The increase in internal energy is  
 $\Delta U = \Delta Q - \Delta W$   
 $= 418 \text{ J} - 40 \text{ J} = 378 \text{ J}$

**Example 16** A gas is compressed from volume  $10 \text{ m}^3$  to  $4 \text{ m}^3$  at constant pressure  $50 \text{ N/m}^2$ . Gas is given 100 J energy by heating then its internal energy.

**Solution.**  $P = 50 \text{ N/m}^2$   
 $dV = 10 - 4 = 6 \text{ m}^3$   
 $\delta W = PdV = 6 \times 50 = 300 \text{ J}$  (Volume is decreasing,  $\delta Q = 100 \text{ J}$ )  
 $W = -300 \text{ J}$   
 $\delta Q = \delta W + dU$   
 $100 + 300 = dU$   
 $dU = \text{increased by } 400 \text{ J}$

**Example 17.** Two moles of a diatomic gas at 300 K are enclosed in a cylinder as shown in figure. Piston is light. Find out the heat given if the gas is slowly heated to 400 K in the following three cases.



- (i) Piston is free to move
- (ii) If piston does not move

- Solution :**
- (iii) If piston is heavy and movable.  
 (i) Since pressure is constant  

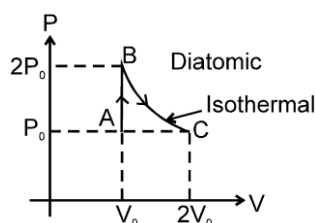
$$\therefore \Delta Q = nC_P \Delta T = 2 \times \frac{7}{2} \times R \times (400 - 300) = 700 R$$
- (ii) Since volume is constant  

$$\therefore \Delta W = 0 \text{ and } \Delta Q = \Delta u \text{ (from first law)}$$

$$\Delta Q = \Delta u = nC_V \Delta T = 2 \times \frac{5}{2} \times R \times (400 - 300) = 500 R$$
- (iii) Since pressure is constant  

$$\therefore \Delta Q = nC_P \Delta T = 2 \times \frac{7}{2} \times R \times (400 - 300) = 700 R$$

**Example 18.** P-V curve of a diatomic gas is shown in the figure. Find the total heat given to the gas in the process AB and BC



**Solution :** From first law of thermodynamics  

$$\Delta Q_{ABC} = \Delta U_{ABC} + \Delta W_{ABC}$$

$$\Delta W_{ABC} = \Delta W_{AB} + \Delta W_{BC} = 0 + nR T_B \ln \frac{V_C}{V_B} = nR T_B \ln \frac{2V_0}{V_0}$$

$$= nRT_B \ln 2 = 2P_0 V_0 \ln 2$$

$$\Delta u = nC_V \Delta T = \frac{5}{2} (2P_0 V_0 - P_0 V_0) \Rightarrow \Delta Q_{ABC} = \frac{5}{2} P_0 V_0 + 2P_0 V_0 \ln 2.$$

**Example 19.** Calculate the value of mechanical equivalent of heat from the following data. Specific heat capacity of air at constant volume = 170 cal/kg-K,  $\gamma = C_p/C_v = 1.4$  and the density of air at STP is 1.29 kg/m<sup>3</sup>. Gas constant R = 8.3 J/mol-K.

**Solution :** Using  $pV = nRT$ , the volume of 1 mole of air at STP is  

$$V = \frac{nRT}{p} = \frac{(1 \text{ mol}) \times (8.3 \text{ J/mol-K}) \times (273 \text{ K})}{1.0 \times 10^5 \text{ N/m}^2} = 0.0224 \text{ m}^3.$$

The mass of 1 mole is, therefore,  

$$(1.29 \text{ kg/m}^3) \times (0.0224 \text{ m}^3) = 0.029 \text{ kg}.$$

The number of moles in 1 kg is  $\frac{1}{0.029}$ . The molar heat capacity at constant volume is

$$C_v = \frac{170 \text{ cal}}{(1/0.029) \text{ mol-K}} = 4.93 \text{ cal/mol-K}.$$

Hence,  $C_p = \gamma C_v = 1.4 \times 4.93 \text{ cal/mol-K}$

or,  $C_p - C_v = 0.4 \times 4.93 \text{ cal/mol-K}$   

$$= 1.97 \text{ cal/mol-K}.$$

Also,  $C_p - C_v = R = 8.3 \text{ J/mol-K}.$

Thus,  $8.3 \text{ J} = 1.97 \text{ cal}.$

The mechanical equivalent of heat is

$$\frac{8.3 \text{ J}}{1.97 \text{ cal}} = 4.2 \text{ J/cal}.$$

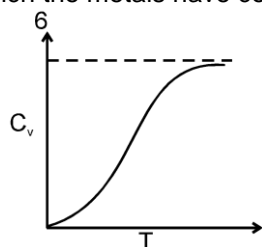


## Average Molar Specific Heat of Metals : [Dulong and Petit law]

At room temperature average molar specific heat of all metals are same and is nearly equal to 3R

( 6 cal. mol<sup>-1</sup> K<sup>-1</sup> ).

[Note : Temp. above which the metals have constant  $C_v$  is called Debye temp.]

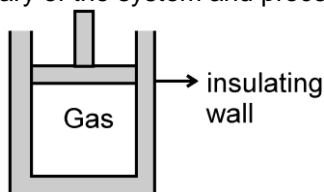


**MAYER'S EQUATION:**

$$C_P - C_V = R \quad (\text{for ideal gases only})$$

## Adiabatic process :

When no heat is supplied or extracted from the system the process is called adiabatic. Process is sudden so that there is no time for exchange of heat. If walls of a container are thermally insulated no heat can cross the boundary of the system and process is adiabatic.



Equation of adiabatic process is given by

$$PV^\gamma = \text{constant} \quad [\text{Poisson Law}]$$

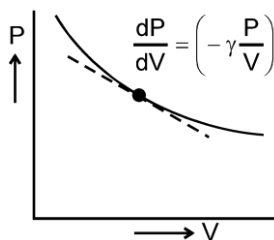
$$T V^{\gamma-1} = \text{constant}$$

$$T V^{\gamma-1} = \text{constant}$$

**Slope of P-V-curve in adiabatic process :**

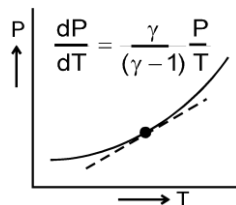
Since  $PV^\gamma$  is a constant

$$\therefore \frac{dP}{dV} = -\gamma \left( \frac{P}{V} \right)$$



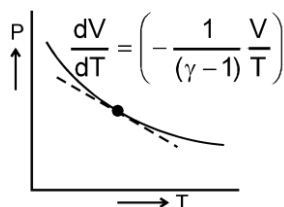
**Slope of P-T-curve in adiabatic process :** Since  $T V^{\gamma-1}$  is a constant

$$\therefore \frac{dP}{dT} = -\frac{\gamma}{(1-\gamma)} \frac{P}{T} = \frac{(\gamma)}{(\gamma-1)} \frac{P}{T}$$



**Slope of T-V-curve :**

$$\frac{dV}{dT} = -\frac{1}{(\gamma-1)} \frac{V}{T}$$



## Work done in adiabatic Process :

$$\Delta W = -\Delta U = nC_v(T_i - T_f) = \frac{P_i V_i - P_f V_f}{(\gamma - 1)} = \frac{nR(T_i - T_f)}{\gamma - 1}$$

work done by system is (+ve) , if  $T_i > T_f$  (hence expansion)

work done on the system is (-ve) if  $T_i < T_f$  (hence compression)

## Solved Examples

**Example 20.** A quantity of air is kept in a container having walls which are slightly conducting. The initial temperature and volume are  $27^\circ\text{C}$  (equal to the temperature of the surrounding) and  $800\text{cm}^3$  respectively. Find the rise in the temperature if the gas is compressed to  $200\text{cm}^3$  (a) in a short time (b) in a long time. Take  $\gamma = 1.4$ .

**Solution :** (a) When the gas is compressed in a short time, the process is adiabatic. Thus,

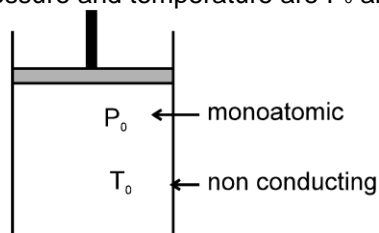
$$T_2 V_2^{\gamma-1} = T_1 V_1^{\gamma-1}$$

$$T_2 = T_1 \left( \frac{V_1}{V_2} \right)^{\gamma-1} = (300 \text{ K}) \times \left[ \frac{800}{200} \right]^{0.4} = 522 \text{ K.}$$

$$\text{Rise in temperature} = T_2 - T_1 = 222 \text{ K.}$$

(b) When the gas is compressed in a long time, the process is isothermal. Thus, the temperature remains equal to the temperature of the surrounding that is  $27^\circ\text{C}$ . The rise in temperature = 0.

**Example 21.** A monoatomic gas is enclosed in a nonconducting cylinder having a piston which can move freely. Suddenly gas is compressed to  $1/8$  of its initial volume. Find the final pressure and temperature if initial pressure and temperature are  $P_0$  and  $T_0$  respectively.



**Solution :** Since process is adiabatic therefore

$$P_0 V_0^{\frac{5}{3}} = P_{\text{final}} \left( \frac{V_0}{8} \right)^{\frac{5}{3}} \Rightarrow \gamma = \frac{C_p}{C_v} = \frac{5R}{2} / \frac{3R}{2} = \frac{5}{3}$$

$$P_{\text{final}} = 32 P_0 .$$

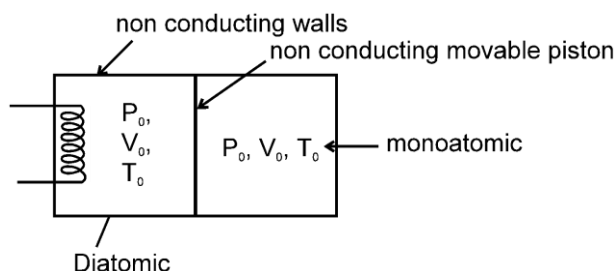
Since process is adiabatic therefore

$$T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1} \Rightarrow T_0 V_0^{2/3} = T_{\text{final}} \left( \frac{V_0}{8} \right)^{2/3} \Rightarrow T = 4T_0$$

**Example 22.** A cylindrical container having nonconducting walls is partitioned in two equal parts such that the volume of the each parts is equal to  $V_0$  . A movable nonconducting piston is kept between the two parts. Gas on left is slowly heated so that the gas on right is compressed upto volume  $\frac{V_0}{8}$  . Find pressure and temperature on both sides if initial pressure and temperature, were  $P_0$



and  $T_0$  respectively. Also find heat given by the heater to the gas. (number of moles in each part is  $n$ )



**Solution :** Since the process on right is adiabatic therefore

$$PV_\gamma = \text{constant}$$

$$\Rightarrow P_0 V_0^\gamma = P_{\text{final}} (V_0/8)^\gamma \Rightarrow P_{\text{final}} = 32 P_0$$

$$T_0 V_0^{\gamma-1} = T_{\text{final}} (V_0/8)^{\gamma-1} \Rightarrow T_{\text{final}} = 4T_0$$

Let volume of the left part is  $V_1$

$$\Rightarrow 2V_0 = V_1 + \frac{V_0}{8} \Rightarrow V_1 = \frac{15V_0}{8}$$

Since number of moles on the left parts remains constant therefore for the left part

$$\frac{PV}{T} = \text{constant.}$$

Final pressure on both sides will be same

$$\Rightarrow \frac{P_0 V_0}{T_0} = \frac{P_{\text{final}} V_1}{T_{\text{final}}} \Rightarrow T_{\text{final}} = 60 T_0$$

$$\Delta Q = \Delta u + \Delta w$$

$$\Delta Q = n \frac{5R}{2} (60T_0 - T_0) + n \frac{3R}{2} (4T_0 - T_0) \Rightarrow \Delta Q = \frac{5nR}{2} \times 59T_0 + \frac{3nR}{2} \times 3T_0$$



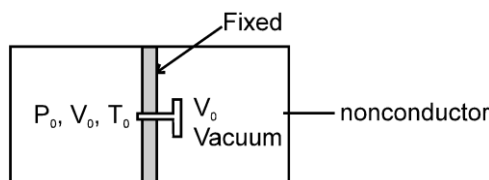
## FREE EXPANSION

If a system, say a gas expands in such a way that no heat enters or leaves the system and also no work is done by or on the system, then the expansion is called the "free expansion".

$\Delta Q = 0$ ,  $\Delta U = 0$  and  $\Delta W = 0$ . Temperature in the free expansion remains constant.

## Solved Example

**Example 23.** A nonconducting cylinder having volume  $2V_0$  is partitioned by a fixed nonconducting wall in two equal part. Partition is attached with a valve. Right side of the partition is a vacuum and left part is filled with a gas having pressure and temperature  $P_0$  and  $T_0$  respectively. If valve is opened find the final pressure and temperature of the two parts.



**Solution :** From the first law thermodynamics  $\Delta Q = \Delta u + \Delta W$

Since gas expands freely therefore  $\Delta W = 0$ , since no heat is given to gas  $\Delta Q = 0$

$\Rightarrow \Delta u = 0$  and temperature remains constant.

$$T_{\text{final}} = T_0$$

Since the process is isothermal therefore  $P_0 \times V_0 = P_{\text{final}} \times 2V_0 \Rightarrow P_{\text{final}} = P_0/2$

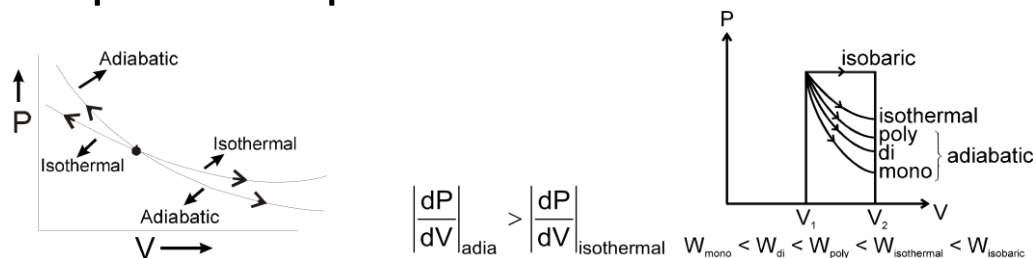


## Reversible and Irreversible Process

A process is said to be reversible when the various stages of an operation in which it is subjected can be traversed back in the opposite direction in such a way that the substance passes through exactly the same conditions at every step in the reverse process as in the direct process.

A process in which any one of the condition stated for reversible process are not fulfilled is called an irreversible process.

## Comparison of slopes of Iso-thermal and Adiabatic Curve



In compression up to same final volume:  $|W_{\text{adia}}| > |W_{\text{isothermal}}|$

In Expansion up to same final volume:  $W_{\text{isothermal}} > W_{\text{adia}}$

## Limitations of 1st Law of Thermodynamics :

The first law of thermodynamics tells us that heat and mechanical work are interconvertible. However, this law fails to explain the following points :

- It does not tell us about the direction of transfer of heat.
- It does not tell us about the conditions under which heat energy is converted into work.
- It does not tell us whether some process is possible or not.

## Mixture of non-reacting gases:

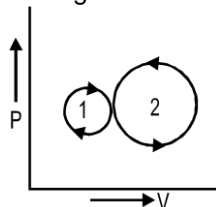
- (a) Molecular weight =  $\frac{n_1 M_1 + n_2 M_2}{n_1 + n_2}$ ,  
 $M_1$  &  $M_2$  are molar masses.
- (b) Specific heat  $C_V = \frac{n_1 C_{V_1} + n_2 C_{V_2}}{n_1 + n_2}$ ,  
 $C_P = \frac{n_1 C_{P_1} + n_2 C_{P_2}}{n_1 + n_2}$ ,  
 $C_{P_{\text{mix}}} = \frac{n_1 C_{P_1} + n_2 C_{P_2} + \dots}{n_1 C_{V_1} + n_2 C_{V_2} + \dots}$
- (c) for mixture,  $\gamma = \frac{C_{P_{\text{mix}}}}{C_{V_{\text{mix}}}}$

## Solved Examples

**Example 24.** 5 gm air is heated from 4°C to 6°C. If the specific heat of air at constant volume is 0.172 cal/gm/°C, then increase in the internal energy of air will be -

**Solution.**  
 $dU = m C_V dT$   
 $dU = 5 \times 0.172 \times 2$   
 $dU = 1.72 \text{ calorie}$

**Example 25.** In the following indicator diagram, the net amount of work done will be -



**Solution.** The cyclic process 1 is clockwise and the process 2 is anti clockwise. Therefore  $W_1$  will be positive and  $W_2$  will be negative area 2 > area 1, Hence the net work will be negative .

**Example 26.** Two gram-mole of a gas, which are kept at constant temperature of 0°C, are compressed from 4 liter to 1 liter. The work done will be

**Solution.**  
 $W = 2.303 \mu RT \log_{10} \frac{V_2}{V_1}$   
 $W = 2.303 \times 2 \times 8.4 \times 273 \log_{10} \frac{1}{4}$

$$W = 2.303 \times 2 \times 8.7 \times 273 \times (\log_{10} - \log_{410})$$

$$\therefore \log_{410} = 0.6021$$

$$\therefore W = -6359 \text{ Joule}$$

**Example 27.** Air is filled in a motor car tube at 27°C temperature and 2 atmosphere pressure. If the tube

$$\left[ \left( \frac{1}{2} \right)^{2/7} = 0.82 \right]$$

suddenly bursts then the final temperature will be

**Solution.**  $T_2 = T_1 \left( \frac{P_2}{P_1} \right)^{\frac{\gamma-1}{\gamma}} \Rightarrow T_2 = 300 \left( \frac{1}{2} \right)^{\frac{0.4}{1.4}} = 300 \left( \frac{1}{2} \right)^{2/7} = 300 \times 0.82 \Rightarrow T_2 = 246 \text{ K}$

**Example 28.** One liter of air at NTP is suddenly compressed to 1 c.c. the final pressure will be.

**Solution.**  $P_2 = P_1 \left( \frac{V_1}{V_2} \right)^{\gamma}$   
 $P_2 = 10^5 (10^3)^{5/3} = 10^5 \times 10^5$   
 $P_2 = 10^{10} \text{ Pascal}$

**Example 29.** In the following fig. the work done by the system in the closed path ABCA is

**Solution.** Work done in closed path ABCA

$$W_{ABCA} = \text{Area of } \Delta ABC = \frac{1}{2} AB \times BC$$

$$W_{ABCA} = -\frac{1}{2} (P_2 - P_1) (V_2 - V_1)$$

**Example 30.** According to the fig. if one mole of ideal gas in cyclic process the work done by the gas in the process will be

**Solution.** Work done  $W = \text{area of PV curve}$

$$= \frac{1}{2} [3P_0 - P_0] [2V_0 - V_0] = P_0 V_0$$

**Example 31.** In above question, heat given by the gas is

**Solution.**  $\delta Q = \mu C_p dT$ ,  $\mu = 1$ ,  $dT = T_A - T_C$ , and for monoatomic ideal gas  $C_p = 5/2 R$

$$\therefore (\delta Q)_{CA} = \frac{5}{2} R [T_A - T_C] = \frac{5}{2} [P_A V_A - P_C V_C]$$

But  $P_A = P_0$ ,  $V_A = V_0$ ,  $V_C = 2V_0$ ,  $P_C = P_0$

$$\frac{PV}{T} = R$$

and

$$\therefore (\delta Q)_{CA} = \frac{5}{2} [P_0 V_0 - P_0 2V_0] = -\frac{5}{2} P_0 V_0$$

**Example 32.** In above question, the heat taken by gas in the path AB will be

**Solution.**  $(\delta Q)_{AB} = \mu C_v dT$  (process is on constant volume)

$$C_v = \frac{3}{2} R, \mu = 1$$

$$(\delta Q)_{AB} = \frac{3}{2} R [T_B - T_A] = \frac{3}{2} [3P_0 V_0 - P_0 V_0]$$

$$= 3P_0 V_0$$

**Example 33.** In above question, the absorbed heat by gas in path BC will be

**Solution.** If the heat given for complete process is  $\delta Q$  then

$$(\delta Q) = (\delta Q)_{AB} + (\delta Q)_{BC} + (\delta Q)_{CA}$$

$dU = 0$  in cyclic process, thus by first law of thermodynamics  $\delta Q = \delta W$

$$\therefore (\delta Q)_{AB} + (\delta Q)_{BC} + (\delta Q)_{CA} = \delta W$$

$$\begin{aligned}
 (\delta Q)_{BC} &= \delta W - (\delta Q)_{AB} - (\delta Q)_{CA} \\
 &= P_0 V_0 + \frac{5}{2} P_0 V_0 - 3P_0 V_0 \\
 &= \frac{P_0 V_0}{2}
 \end{aligned}$$

**Example 34.** For a given cyclic process as shown in fig. the magnitude of absorbed energy for the system is

**Solution.** In cyclic process  
 $Q = W$  ( $\because dU = 0$ )  
 $Q = \text{area of closed loop}$   
 $Q = 102\pi \text{ Joule}$



### SECOND LAW OF THERMODYNAMICS

This law gives the direction of heat flow.

**According to Classius :** It is impossible to make any such machine that can transfer heat from an object with low temperature to an object with high temperature without an external source.

**According to Kelvin :** It is impossible to obtain work continuously by cooling an object below the temperature of its surroundings.

**Statement of Kelvin-Planck :** It is impossible to construct any such machine that works on a cyclic process and absorbs heat from a source, converts all that heat into work and rejects no heat to sink.

**Heat engine :**

The device, used to convert heat energy into mechanical energy, is called a heat engine.

For conversion of heat into work with the help of a heat engine, the following conditions have to be met with

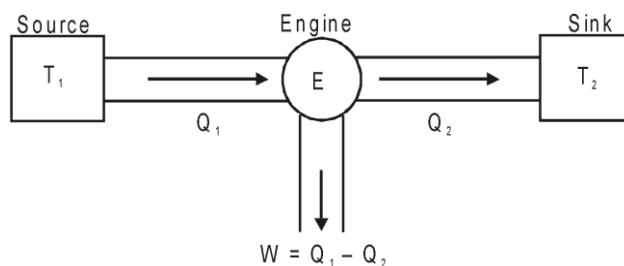
There should be a body at higher temperature ' $T_1$ ' from which heat is extracted. It is called the source.

Body of the engine containing working substance.

There should be a body at lower temperature ' $T_2$ ' to which heat can be rejected. This is called the sink.

**Working of heat engine :**

Schematic diagram of heat engine



Engine derives an amount ' $Q_1$ ' of heat from the source.

A part of this heat is converted into work ' $W$ '.

Remaining heat ' $Q_2$ ' is rejected to the sink.

Thus  $Q_1 = W + Q_2$

or the work done by the engine is given by  $W = Q_1 - Q_2$

**Efficiency of heat engine :**

Efficiency of heat engine ( $\eta$ ) is defined as the fraction of total heat, supplied to the engine which is converted into work.

Mathematically

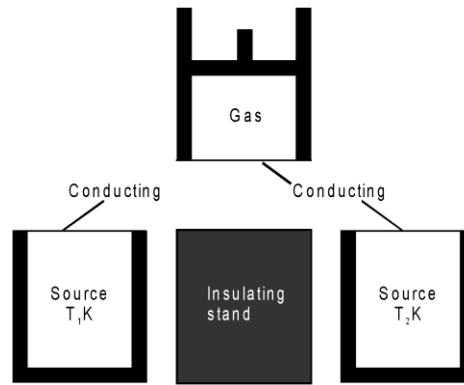
$$\eta = \frac{W}{Q_1} \quad \text{or} \quad \eta = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

### CARNOT ENGINE AND CARNOT CYCLE

**Carnot engine :**

Carnot engine is an ideal heat engine. It consists of the following parts.

**Schematic diagram :**



**Source :** It is a reservoir of heat energy with a conducting top maintained at a constant temperature  $T_1K$ . Source is so big that extraction of any amount of heat from it does not change its temperature.

**Body of heat engine :** It is a barrel having perfectly insulating walls and conducting bottom. It is fitted with an air tight piston capable of sliding within the barrel without friction. The barrel contains some quantity of an ideal gas.

**Sink :** It is a huge body at a lower temperature  $T_2$  having a perfectly conducting top. The size of the sink is so large that any amount of heat rejected to it does not increase its temperature.

**Insulating stand :** It is a stand made up of perfectly insulating material such that the barrel when placed over it becomes thoroughly insulated from the surroundings.

**Carnot cycle :**

As the engine works, the working substance of the engine undergoes a cycle known as Carnot cycle. The Carnot cycle consists of the following four strokes.

**Graphical representation of Carnot cycle :**

**First stroke (Isothermal expansion) :**

In this stroke the barrel is placed over the source. The piston is gradually pushed back as the gas expands. Fall of temperature, due to expansion, is compensated by the supply of heat from the source and consequently temperature remains constant. The conditions of the gas change from  $A(P_1, V_1)$  to  $B(P_2, V_2)$ . If  $W_1$  is the work done during this process, then heat  $Q_1$  derived from the source is given by

$$Q_1 = W_1 = \text{Area ABGE} = RT \log_e \left( \frac{V_2}{V_1} \right)$$

**Second stroke (Adiabatic expansion) :**

The barrel is removed from the source and is placed over the insulating stand. The piston is pushed back so that the gas expands adiabatically resulting in fall of temperature from  $T_1$  to  $T_2$ . The conditions of the gas change from  $B(P_2, V_2)$  to  $C(P_3, V_3)$ . If  $W_2$  is the work done in this case then

$$W_2 = \text{Area BCHG} = \frac{R}{\gamma - 1} (T_1 - T_2)$$

**Third stroke (isothermal compression) :**

The barrel is placed over the sink. Piston is pushed down there by compressing the gas. The heat generated due to compression flows to the sink maintaining the temperature of the barrel constant. The state of the gas change from  $C(P_3, V_3)$  to  $D(P_4, V_4)$ . If  $W_3$  is the work done in this process and  $Q_2$  is the heat rejected to the sink, then

$$Q_2 = W_3 = \text{Area CDFH} = RT_2 \log_e \left( \frac{V_3}{V_4} \right)$$

**Fourth stroke (Adiabatic compression) :**

The barrel is placed over the insulating stand. The piston is moved down thereby compressing the gas adiabatically till the temperature of gas increases from  $T_2$  to  $T_1$ . The state of gas changes from  $D(P_4, V_4)$  to  $A(P_1, V_1)$ . If  $W_4$  is the work done in this process, then

$$W_4 = \text{Area ADFE} = \frac{R}{\gamma - 1} (T_1 - T_2)$$

**Heat converted into work in Carnot cycle :**

During the four strokes,  $W_1$  and  $W_2$  are the work done by the gas and  $W_3$  and  $W_4$  are the work done on the gas. Therefore the net, work performed by the engine

$$W = W_1 + W_2 - W_3 - W_4 = \text{Area ABGE} + \text{Area BCHG} - \text{Area CDFH} - \text{Area ADEF} = \text{Area ABCD}$$

Thus net work done by the engine during one cycle is equal to the area enclosed by the indicator diagram

$$W = R(T_1 - T_2) \log_e \left( \frac{V_2}{V_1} \right)$$

of the cycle. Analytically

**Efficiency of Carnot engine :**

Efficiency ( $\eta$ ) of an engine is defined as the ratio of useful heat (heat converted into work) to the total heat supplied to the engine. Thus.

$$\eta = \frac{W}{Q_1} = \frac{Q_1 - Q_2}{Q_1} \quad \text{or} \quad \eta = \frac{R(T_1 - T_2) \log_e \left( \frac{V_2}{V_1} \right)}{RT_1 \log_e \left( \frac{V_2}{V_1} \right)} = \frac{T_1 - T_2}{T_1} \quad \text{or} \quad \eta = 1 - \frac{Q_2}{Q_1} = 1 - \frac{T_2}{T_1}$$

**Some important points regarding Carnot engine**

Efficiency of an engine depends upon the temperatures between which it operates.

$\eta$  is independent of the nature of working substance.

$\eta$  is one only if  $T_2 = 0$ . Since absolute zero is not attainable, hence even an ideal engine cannot be 100 % efficient.

$\eta$  is one only if  $Q_2 = 0$ . But  $\eta = 1$  is never possible even for an ideal engine. Hence  $Q_2 \neq 0$ .

Thus it is impossible to extract heat from a single body and convert the whole of it into work.

If  $T_2 = T_1$ , then  $\eta = 0$

In actual heat engines, there are many losses due to friction etc. and various processes during each cycle are not quasistatic, so the efficiency of actual engines is much less than that of an ideal engine.

### Solved Examples

**Example 35.** A Carnot engine has same efficiency between (i) 100 K and 500K and (ii) T and 900 K. The value of T is

**Solution.** Efficiency  $\eta = 1 - \frac{T_2}{T_1}$

$$\text{or} \quad \eta = 1 - \frac{100}{500} = 1 - \frac{T}{900} \quad \text{or} \quad \frac{100}{500} = \frac{T}{900} \quad \therefore T = 180\text{K}$$

**Example 36.** A Carnot engine takes  $10^3$  kilocalories of heat from a reservoir at  $627^\circ\text{C}$  and exhausts it to a sink at  $27^\circ\text{C}$ . The efficiency of the engine will be.

**Solution.** Efficiency of Carnot engine

$$\eta = 1 - \frac{T_2}{T_1} = 1 - \frac{300}{900} = \frac{2}{3} \quad \text{or} \quad \eta = 66.6\%$$

**Example 37.** In the above problem, the work performed by the engine will be

**Solution.** Work performed by the engine

$$W = \eta Q_1 = \frac{2}{3} \times 10^6 \times 4.2 \quad \text{or} \quad W = 2.8 \times 10^6 \text{ Joule}$$

**Example 38.** A Carnot engine has an efficiency of 40% when the sink temperature is  $27^\circ\text{C}$ . The source temperature will be

**Solution.**  $\eta_{\text{efficiency}} = 1 - \frac{T_2}{T_1}$  or  $\frac{2}{5} = 1 - \frac{300}{T_1} \quad \therefore T_1 = 500\text{K}$

**Example 39.** A reversible engine takes heat from a reservoir at  $527^\circ\text{C}$  and gives out to the sink at  $127^\circ\text{C}$ . The engine is required to perform useful mechanical work at the rate of 750 watt. The efficiency of the engine is

**Solution.** Efficiency  $\eta = 1 - \frac{T_2}{T_1}$  or  $\eta = 1 - \frac{400}{800} = \frac{1}{2}$  or  $\eta = 50\%$

**Example 40.** The efficiency of Carnot's engine is 50%. The temperature of its sink is  $7^\circ\text{C}$ . To increase its efficiency to 70%. The increase in heat of the source will be

## Kinetic Theory of Gases & Thermodynamics

**Solution.**

Efficiency in first state  $\eta = 50\% = 1/2$

$$T_2 = 273 + 7 = 280 \text{ K}$$

$$\text{Formula } \eta = 1 - \frac{T_2}{T_1} \quad \frac{1}{2} = 1 - \frac{280}{T_1} \Leftrightarrow \frac{280}{T_1} = \frac{1}{2}$$

or  $T_1 = 560^\circ\text{K}$  (temperature of source)

$$\text{In the second state (i) } \frac{70}{100} = 1 - \frac{280}{T_1}$$

$$T_1 = \frac{2800}{3} = 933.3\text{K}$$

$\therefore$

$$\therefore \text{ Increase in source temperature} = (933.3 - 560) = 373.3 \text{ K}$$

**Example 41.** A Carnot's engine work at  $200^\circ\text{C}$  and  $0^\circ\text{C}$  and another at  $0^\circ\text{C}$  and  $-200^\circ\text{C}$ . The ratio of efficiency of the two is

$$\eta = \frac{(T_1 - T_2)}{T_1}$$

**Solution.**

$$\eta_1 = \frac{(473 - 273)}{473} = \frac{200}{473} \quad \text{and} \quad \eta_2 = \frac{(273 - 73)}{273} = \frac{200}{273}$$

$$\frac{\eta_1}{\eta_2} = \frac{273}{473} = 0.577$$

**Example 42.** A Carnot engine work as refrigerator in between  $0^\circ\text{C}$  and  $27^\circ\text{C}$ . How much energy is needed to freeze 10 kg ice at  $0^\circ\text{C}$ .

**Solution.**

Heat absorbed by sink

$$Q_2 = 10 \times 10^3 \times 80 = 800 \text{ k.cal}$$

$$\text{Now } \frac{Q_1}{Q_2} = \frac{T_1}{T_2}, \quad Q_1 = Q_2 \cdot \frac{T_1}{T_2}$$

$$\therefore Q_1 = 800 \times \frac{300}{273} \text{ k.cal} = 879 \text{ kcal}$$

**Example 43.** Work efficiency coefficient in above question

**Solution.**

Work efficiency coefficient (coefficient of performance)

$$\beta = \frac{Q_2}{Q_1 - Q_2} = \frac{800 \times 10^3}{(879 - 800) \times 10^3} = 10.13$$

**Example 44.** A Carnot engine works as a refrigerator in between 250K and 300K. If it acquires 750 calories from heat source at low temperature, then the heat generated at higher temperature. (in calories) will be.

$$\text{Solution . } \eta = \frac{Q_2}{Q_1 - Q_2} = \frac{T_2}{T_1 - T_2} \Rightarrow \frac{750}{Q_1 - 750} = \frac{250}{300 - 250}$$

$$Q_1 = 900 \text{ Calories}$$

## Solved Miscellaneous Problems

**Problem 1.** A vessel of volume  $2 \times 10^{-2} \text{ m}^3$  contains a mixture of hydrogen and helium at  $47^\circ\text{C}$  temperature and  $4.15 \times 10^5 \text{ N/m}^2$  pressure. The mass of the mixture is  $10^{-2} \text{ kg}$ . Calculate the masses of hydrogen and helium in the given mixture.

**Solution:**

Let mass of  $\text{H}_2$  is  $m_1$  and  $\text{He}$  is  $m_2$

$$\therefore m_1 + m_2 = 10^{-2} \text{ kg} = 10 \times 10^{-3} \dots (1)$$

Let  $P_1$ ,  $P_2$  are partial pressure of  $\text{H}_2$  and  $\text{He}$

$$P_1 + P_2 = 4.15 \times 10^5 \text{ N/m}^2$$

for the mixture

$$(P_1 + P_2) V = \left( \frac{m_1}{n_1} + \frac{m_2}{n_2} \right) RT$$

$$\Rightarrow 4.15 \times 10^5 \times 2 \times 10^{-2} = \left( \frac{m_1}{2 \times 10^{-3}} + \frac{m_2}{4 \times 10^{-3}} \right) 8.31 \times 320$$

$$\Rightarrow \frac{m_1}{2} + \frac{m_2}{4} = \frac{4.15 \times 2}{8.31 \times 320} = 0.00312 = 3.12 \times 10^{-3}$$

$$\Rightarrow 2m_1 + m_2 = 12.48 \times 10^{-3} \text{ kg} \quad \dots(2)$$

Solving (1) and (2)

$$m_1 = 2.48 \times 10^{-3} \text{ kg} \cong 2.5 \times 10^{-3} \text{ kg}$$

and  $m = 7.5 \times 10^{-3} \text{ kg}.$

**Problem 2.** The pressure in a monoatomic gas increases linearly from  $4 \times 10^5 \text{ N m}^{-2}$  to  $8 \times 10^5 \text{ N m}^{-2}$  when its volume increases from  $0.2 \text{ m}^3$  to  $0.5 \text{ m}^3$ . Calculate the following:

- (a) work done by the gas.  
(b) increase in the internal energy.

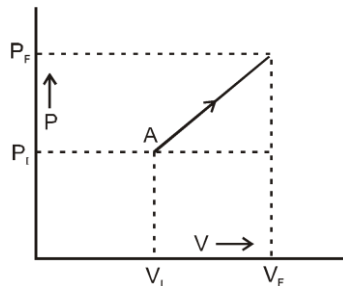
**Solution :** (a) As here pressure is varying linearly with volume, work done by the gas

$$\Delta W = \int P dV = \text{area under P-V curve}$$

which in the light of figure 1 becomes:

$$\Delta W = P_i (V_F - V_i) (P_F - P_i) \times (V_F - V_i)$$

$$\text{i.e., } \Delta W = P_i (V_F - V_i) + \frac{1}{2} (P_F - P_i) \times (V_F - V_i)$$



$$\text{i.e., } \Delta W = \frac{1}{2} (0.5 - 0.2) (8 + 4) \times 10^5$$

$$\text{i.e., } \Delta W = 1.8 \times 10^5 \text{ J}$$

(b) The change in internal energy of a gas is given by

$$\Delta U = \mu C_v \Delta T = \frac{\mu R \Delta T}{(\gamma - 1)} = \frac{(P_F V_F - P_i V_i)}{(\gamma - 1)}$$

As the gas is monatomic  $\gamma = (5/3)$

$$\text{So, } \Delta U = \frac{10^5 (8 \times 0.5 - 4 \times 0.2)}{[(5/3) - 1]} = \frac{3}{2} \times 10^5 (4 - 0.8).$$

$$\text{i.e., } \Delta U = 4.8 \times 10^5 \text{ J}$$

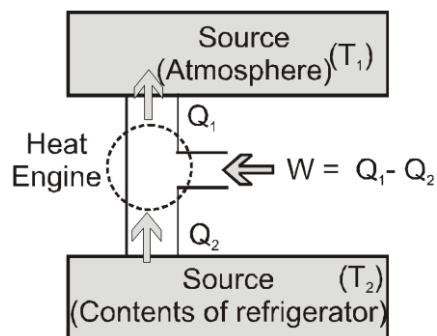
## Refrigerator or Heat Pump

A refrigerator or heat pump is basically a heat engine run in reverse direction.

It essentially consists of three parts

- (1) **Source** : At higher temperature  $T_1$ .
- (2) **Working substance** : It is called refrigerant liquid ammonia and freon works as a working substance
- (3) **Sink** : At lower temperature  $T_2$ .





The working substance takes heat  $Q_2$  from a sink (contents of refrigerator) at lower temperature, has a net amount of work done  $W$  in it by an external agent (usually compressor of refrigerator) and gives out a larger amount of heat  $Q_1$  to a hot body at temperature  $T_1$  (usually atmosphere). Thus, it transfers heat from a cold to a hot body at the expense of mechanical energy supplied to it by an external agent. The cold is thus cooled more and more.

The performance of a refrigerator is expressed by means of "coefficient of performance"  $\beta$  which is defined as the ratio of the heat extracted from the cold body to the needed to transfer it to the hot body.

$$\beta = \frac{\text{Heat extracted}}{\text{Work done}} = \frac{Q_2}{W} = \frac{Q_2}{Q_1 - Q_2}$$

i.e.

A perfect refrigerator is one which transfers heat from cold to hot body without doing work

i.e.  $W = 0$  so that  $Q_1 = Q_2$  hence  $\beta = \infty$

(1) **Carnot refrigerator:**

$$\text{For Carnot refrigerator } \frac{Q_1}{Q_2} = \frac{T_1}{T_2} \Rightarrow \frac{Q_1 - Q_2}{Q_2} = \frac{T_1 - T_2}{T_2} \text{ or } \frac{Q_2}{Q_1 - Q_2} = \frac{T_2}{T_1 - T_2}$$

$$\beta = \frac{T_2}{T_1 - T_2}$$

So Coefficient of performance

here  $T_1$  = temperature of surrounding  $T_2$  = temperature of cold body. It is clear that  $\beta = 0$  when  $T_2 = 0$  i.e. the coefficient of performance will be zero if the cold body is at the temperature equal to absolute zero.

(2) **Relation between coefficient of performance and efficiency of refrigerator**

$$\beta = \frac{Q_2}{Q_1 - Q_2} = \frac{Q_2 / Q_1}{1 - Q_2 / Q_1} \quad \dots\dots\dots(i)$$

$$\text{But the efficiency } \eta = \frac{Q_2}{Q_1} \text{ or } \frac{Q_2}{Q_1} = 1 - \eta \quad \dots\dots\dots(ii)$$

Form (i) and (ii) we get ,  $\eta$

(3) **Entropy**

Entropy is measure of disorder of molecular motion of a system. Greater is the disorder, greater is the entropy.

The change in entropy i.e

$$dS = \frac{\text{Heat absorbed by system}}{\text{Absolute temperature}} \text{ or } dS = \frac{dQ}{T}$$

The relation is called the mathematical form of Second Law of Thermodynamics.

(1) **For solids and liquids**

(i) When heat given to a substance change its state at constant temperature, then change in entropy

$$dS = \frac{dQ}{T} = \pm \frac{mL}{T}$$

where positive sign refers to heat absorption and negative sign to heat evolution.

(ii) When heat given to substance raises its temperature from  $T_1$  to  $T_2$  then change in entropy

$$dS = \int \frac{dQ}{T} = \int_{T_1}^{T_2} mc \frac{dT}{T} = mc \log_e \left( \frac{T_2}{T_1} \right) \Rightarrow \Delta S = 2.303 mc \log_{10} \left( \frac{T_2}{T_1} \right)$$

**(2) For a perfect gas :** Perfect gas equation for n moles is  $PV = nRT$

$$\Delta S = \int \frac{dQ}{T} = \int \frac{\mu C_V dT + P dV}{T} \quad [\text{As } dQ = dU + dW]$$

$$\Rightarrow \Delta S = \int \frac{\mu C_V dT + \frac{\mu RT}{V} dV}{T} = \mu C_V \int_{T_1}^{T_2} \frac{dT}{T} + \mu R \int_{V_1}^{V_2} \frac{dV}{V} \quad [\text{As } PV = \mu RT]$$

$$\therefore \Delta S = \mu C_V \log_e \left( \frac{T_2}{T_1} \right) + \mu R \log_e \left( \frac{V_2}{V_1} \right)$$

$$\text{In terms of T and P, } \Delta S = \mu C_P \log_e \left( \frac{T_2}{T_1} \right) - \mu R \log_e \left( \frac{P_2}{P_1} \right)$$

$$\text{and in terms of P and V } \Delta S = \mu C_V \log_e \left( \frac{P_2}{P_1} \right) + \mu C_P \log_e \left( \frac{V_2}{V_1} \right)$$