

HEAT - II

EXERCISE – I

SINGLE CORRECT

1. B

Law $P \propto r$ and high temperature

2. C

Speed of molecules changes randomly due to collision but average speed remain constant.

3. B

Since net force is zero over the system at rest hence momentum will be zero.

4. A

$$\sqrt{\frac{3R T_{O_2}}{M_{O_2}}} = \sqrt{\frac{3R T_{N_2}}{M_{N_2}}}$$

$$T_{O_2} = \frac{M_{O_2}}{M_{N_2}} \cdot T_{N_2}$$

$$= \frac{16}{14} \times 373 = 426.3K$$

5. C

$$V_{avg} = \frac{V_1 + V_2 + \dots + V_n}{n}$$

$$V_{rms} = \sqrt{\frac{V_1^2 + V_2^2 + \dots + V_n^2}{n}}$$

For one particle $n = 1$

$$V_{avg} = V_{rms} = V_1$$

6. C

$$V_{rms_{O_2}} = \sqrt{\frac{3RT_{O_2}}{M_{O_2}}}$$

$$V_{rmsO} = \sqrt{\frac{3RT_{O_2} \times 2}{M_{O_2}/2}} = 2\sqrt{\frac{3RT_{O_2}}{M_{O_2}}} = 2V$$

7. B

$$V_{avg} \propto \frac{1}{\sqrt{M_0}}$$

$$\& M_0 > M_{H_2} \therefore V_{avgO} < V_{avg.H_2}$$

8. A

$$V_{rms} = \sqrt{\frac{3RT}{M}}$$

$$V_{MP} = \sqrt{\frac{2RT}{M}}$$

$$V_{av} = \sqrt{\frac{8RT}{\pi M}}$$

$$V_S = \sqrt{\frac{5RT}{3M}}$$

$$\therefore V_{rms} > V_{av} > V_{MP} > V_S$$

9. B

$$V_{av} = \sqrt{\frac{8RT}{\pi M}}$$

Independent of other gas.

10. C

$$PV = nRT$$

$$P = \frac{nRT}{V} = \text{const.}$$

11. A

$$\text{R.M.S. speed} = \sqrt{\frac{(2^2 + 10^2 + 11^2)}{2}} u^2$$

$$= 8.66 u$$

$$\text{Mean speed} = \frac{(2 + 10 + 11)}{3} u$$

$$= 7.66 u$$

12. D

$$V_{avg} = \frac{1 + 2 + 3 + \dots + N}{N} = \frac{N(N+1)}{2N}$$

$$= \frac{(N+1)}{2}$$

$$V_{rms} = \sqrt{\frac{1^2 + 2^2 + \dots + N^2}{N}} = \sqrt{\frac{2N+1}{3}}$$

$$\frac{V_{rms}}{V_{avg}} = \frac{2}{(N+1)} \sqrt{\frac{2N+1}{3}}$$

13. D

Data Insufficient

 $\therefore$ direction not given

14. C

Isothermally $\Rightarrow$ internal energy remain constant.But volume $\downarrow \Rightarrow$ no. of collisions per unit area with walls of container increases.

15. A

$$\text{Avg rotational K.E.} = \frac{1}{2} kT \times 2 = kT$$

So it will be same for both

16. D**17. D**

$$U_1 + U_2 = U_{\text{mixture}}$$

$$\frac{3}{2} R [n_1 T_1 + n_2 T_2] = \frac{3}{2} R [n_1 + n_2] T_{\text{mix}}$$

$$T_{\text{mix}} = \left[\frac{n_1 T_1 + n_2 T_2}{n_1 + n_2} \right] \frac{N_A}{N_A}$$

18. Bfor $L \rightarrow M$

$$P = \text{const.} \Rightarrow T = \frac{P}{nR} V$$

a st. line with +ve slope.

19. D

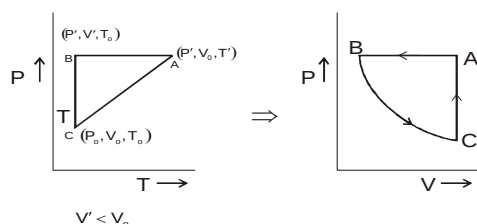
$$\frac{P}{T} = \text{const.} = \frac{nR}{V}$$

but V is different, So slope is different.**20. C**

$$PT = \text{const.}$$

$$P \left(\frac{PV}{nR} \right) = \text{const.}$$

$$P^2 V = \text{const.}$$

21. C**22. A**

$$V_{\text{av}} \propto \sqrt{T} \propto \sqrt{PV}$$

$$V_{\text{av}_1} : V_{\text{av}_2} : V_{\text{av}_3}$$

$$\sqrt{V_0 P_0} : \sqrt{V_0 \cdot 4P_0} : \sqrt{4V_0 P_0}$$

$$1 : 2 : 2$$

23. D

$$PV = nRT$$

$$= n N_0 kT$$

$$\frac{PV}{kT} = n N_0 = \text{no. of molecules}$$

24. D

$$\frac{MKT}{PV} = \frac{MKT}{nRT} = \frac{M_0}{N_A}$$

Depend upon Nature of gas

25. A

$$PV = \frac{2}{3} K.E.$$

$$E = \frac{3}{2} nRT$$

(Translational K.E. for all the particle)

26. C**27. A**

$$PV = nRT$$

$$n = \frac{PV}{RT} = \frac{1.3 \times 10^5 \times \left[7 \times (10^{-2})^3 \times 10^3 \right]}{8.3 \times 273}$$

So, No of molecules

$$= \frac{1.3 \times 10^5 \times 7 \times 10^{-3}}{8.3 \times 273} \times 6.023 \times 10^{23}$$

$$2.4 \times 10^{23}$$

28. B

$$PV = \frac{4}{M_{\text{Ar}}} \cdot RT \quad \text{--- (1)}$$

$$\text{Now, } PV = \frac{(4 - .8)}{M_{\text{Ar}}} R (T + 50) \quad \text{--- (2)}$$

$$(1) \& (2) \Rightarrow (4 - .8)(T + 50) = 4T$$

$$4T - .8T + 200 - .8 \times 50 = 4T$$

$$T = \frac{200 - .8 \times 50}{.8}$$

$$T = 200 \text{ K}$$

29. A**30. C**

$$PV = nRt \quad \text{--- (1)}$$

$$P \left(\frac{P_0/2 - P_0}{2V_0 - V_0} \right) V + \frac{3P_0}{2} \quad \text{--- (2)}$$

$$(1) \& (2) \Rightarrow \left(\frac{3}{2} P_0 - \frac{P_0 V}{2V_0} \right) V = nRT$$

$$\frac{dT}{dV} = 0 \Rightarrow \frac{3}{2} P_0 - \frac{P_0 V}{V_0} = 0$$

$$V = \frac{3}{2} V_0$$

$$T_{\max} = \left(\frac{3}{2} P_0 - \frac{P_0}{2 V_0} \cdot \frac{3}{2} V_0 \right) \frac{3}{2} V_0 \cdot \frac{1}{nR}$$

$$= \frac{6}{4} P_0 \cdot \frac{3}{2} V_0 \cdot \frac{1}{R}$$

$$= \frac{9 P_0 V_0}{FR}$$

31. B

Initially

$$PV_1 = \frac{12}{M} R T_1$$

or

$$P(4 \times 10^{-3}) = \frac{12}{M} R (273 + 7)$$

$$A = \frac{m}{V_2} = \frac{12}{V_2} = 6 \times 10^{-4} \text{ gm/cc}$$

$$P \left(\frac{12}{6 \times 10^{-4}} \right) \times (10^{-2})^3 = \frac{12}{M} R (T) \text{ — (2)}$$

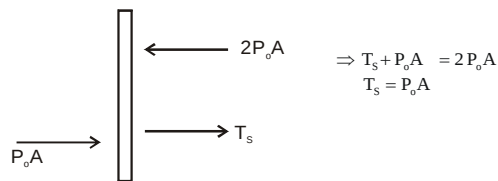
from 1 ÷ 2

$$\frac{4 \times 10^{-3}}{12 \times 10^{-6}} \times 6 \times 10^{-4} = \frac{273 + 7}{T}$$

$$T = 1400 \text{ K}$$

32. B**33. A****34. C** $V = \text{const.}$ $T = \text{doubled}$

$$p = 2P_0$$

**35. A**

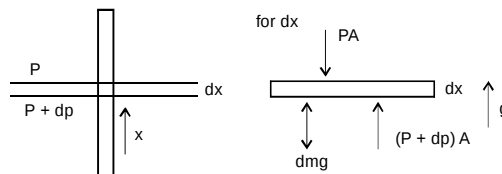
$$pV^{2/3} = \text{const.}$$

$$\frac{nRT}{v} v^{2/3} = \text{const.}$$

$$T v^{2/3-1} = \text{const.}$$

$$T \cdot v^{-1/3} = \text{const.}$$

$$\text{So, } V \uparrow = T \uparrow$$

36. C

$$(p + dp) A - dm g - PA = dm g$$

$$Adp = 2dm g$$

$$Adp = 2\rho_x A dx g$$

$$dp = 2\rho_x g dx$$

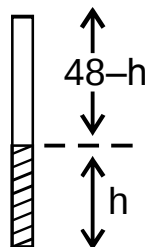
$$= \frac{PM}{RT}$$

$$dp = \frac{2PM}{RT} \cdot g \cdot dx$$

$$\int_{p_0}^{p'_0} dp/p = \frac{2Mg}{RT} \int_0^{x=x/2} dx$$

$$\ln \frac{p'_0}{p_0} = \frac{2Mg}{RT} \cdot \frac{x}{2}$$

$$\frac{p'_0}{p_0} = e^{MgH/RT}$$

37. C

$$P + h = 76$$

$$P_1 V_1 = P_2 V_2$$

$$76.5 = P(48 - h)$$

$$(76 - h)(4 - h)$$

$$h = 38 \text{ cm}$$

$$\text{so, } 48 - h = 10 \text{ cm} = .1 \text{ m}$$

38. A

$$P + 50 = 75$$

$$P = 25 \text{ cm of } H_g$$

$$\frac{10^5}{75} \times 25$$

$$= 33.3 \text{ kPa}$$

39. D

$$\text{Total energy} = 100 + 200$$

$$= 300 \text{ J}$$

40. B

$$W = \int_{V_1}^{V_2} PdV$$

$$\begin{aligned}
 &= \int_{V_1}^{V_2} aV^2 dV \\
 &= a \left[\frac{V^3}{3} \right]_{V_1}^{V_2} = \frac{a}{3} (V_2^3 - V_1^3) \\
 &= \frac{1}{3} [P_2 V_2 - P_1 V_1] \\
 &= \frac{1}{3} [nR\Delta T] = \frac{1}{3} R (T_2 - T_1)
 \end{aligned}$$

41. D

In RS & SP Volume has decreased

42. A

W = Area Under the Curve

43. C

$$W = P\Delta V$$

$$\Delta V_1 = \Delta V_2 \quad \& \quad P_1 < P_2$$

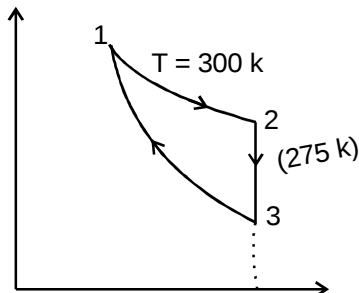
$$\Rightarrow W_1 < W_2$$

44. A

All the three things for a fixed mass of an ideal gas only depends upon temp.

45. A

W = Area Under the Curve

46. A

$$\Delta Q_{1-2} = \Delta W_{1-2}$$

$$\Delta Q_{2-3} = \Delta U_{2-3} = -40 \text{ J}$$

$$\Rightarrow \Delta W_{2-3} = 0$$

$$\Delta Q_{3-1} = 0$$

$$\Delta U_{3-1} = n c_v (300 - 275)$$

$$\Delta Q_T = \Delta W_T$$

$$\Delta Q_{3-1} + \Delta Q_{2-3} + \Delta Q_{1-2}$$

$$= \Delta W_{1-2} + \Delta W_{2-3} + \Delta W_{3-1}$$

$$\Delta Q_{2-3} - \Delta W_{2-3} = \Delta W_{3-1}$$

$$\Delta W_{3-1} = -40 \text{ J}$$

47. B

$$\Delta Q = \Delta U + \Delta W$$

$$\Delta U = \Delta Q - \Delta W$$

$$Q - P_o \Delta V$$

$$Q - P_o \left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right)$$

48. D

$$V = KT$$

$$\frac{dV}{dT} = K \Rightarrow \frac{d^2V}{dT^2} = 0$$

49. D

$$W_{\text{net}} = W_{1-2} + W_{2-3} + W_{3-1}$$

$$10 = W_{1-2} + 0 - 20$$

$$W_{1-2} = 30 \text{ J}$$

$$\Delta U_{1-2} = 0$$

$$\therefore \Delta Q_{1-2} = \Delta W_{1-2} + \Delta U_{1-2}$$

$$= 30 \text{ J}$$

50. D ΔU is a state function**51. D**

$$\Delta U_{ab} = \Delta Q_{acp} - \Delta W_{acb}$$

$$= 200 - 80 = 120 \text{ J}$$

$$\Delta W_{adb} = \Delta Q_{adb} - \Delta U_{ab}$$

$$= 144 - 120 = 24 \text{ J}$$

52. B

$$\Delta Q_{ba} = \Delta W_{ba} + \Delta U_{ba}$$

$$= -52 \text{ J} - 120 \text{ J}$$

$$= 172 \text{ J}$$

53. D

$$\Delta U_{ab} = U_b - U_a$$

$$U_b = 120 + 40 = 160 \text{ J}$$

54. B

$$\Delta Q_{db} = \Delta U_{db} + \Delta W_{db} \quad (v = \text{const.})$$

$$= U_b - U_d$$

$$= 160 - 88 = 72 \text{ J}$$

55. B

For AB

$$\Delta U = 0 \quad (T = \text{const.})$$

$$\Delta W = nRT \ln \frac{V_2}{V_1} = nRT \ln \frac{P_1}{P_2}$$

$$= -Ve (\because P_1 < P_2)$$

$$\Delta Q = \Delta U + \Delta W = -ve$$

(Heat is rejected)

$$\text{For BC } \therefore T \downarrow \quad \therefore U \downarrow$$

56. B

for isothermal process

$$T = \text{const.}$$

$$\therefore U = \text{const.} \quad \text{or} \quad \Delta U = 0$$

$$\Delta W = \Delta Q$$

$$= +ve$$

57. A, C

$$\Delta U \text{ for a cyclic process} = 0$$

58. D ΔU will be same for both the process

$$\Rightarrow \Delta Q - \Delta W \text{ will be same}$$

59. A

$$\Delta Q = \Delta W + 3\Delta W$$

$$= 4\Delta W$$

$$\therefore n = \frac{\Delta W}{\Delta Q} = \frac{\Delta W}{4\Delta W} = 0.25$$

60. A

$$C_v = \frac{f}{2} \cdot R = \frac{5}{2} R$$

61. B

Work is done during expansion by the gas against external pressure.

62. C

$$C = \frac{fR}{2} + \frac{W_{\text{gas}}}{n\Delta T}$$

$$C = C_v + \frac{W_{\text{gas}}}{n\Delta T} \quad \therefore C > C_v$$

63. C

$$C_p = C_v + \frac{W_{\text{gas}}}{n\Delta T}$$

$$C_p - C_v = R \text{ is for ideal gas}$$

64. B

$$f_{\text{translational}} = 3 \text{ (always)}$$

65. A

$$\frac{1}{2}mv^2 = nC_v dT$$

$$\frac{1}{2}mv^2 = \frac{m}{.03} \left(\frac{5}{2} R \right) \Delta T$$

$$\Delta T = \frac{.03 \times 100^4}{5R} = \frac{6 \times 10^{-3} \times 10^4}{R}$$

$$= \frac{60}{R}$$

66. D

$$\frac{\text{Total Mass}}{\text{Total No. of moles}}$$

$$= \frac{n_1 m_1 + n_2 m_2}{(n_1 + n_2)} = \frac{(5 \times 4) + (2 \times 2)}{(5 + 2)}$$

$$= \frac{24}{7}$$

67. AHe - monoatomic H_2 - diatomic

$$f = 3$$

$$f = 5$$

$$f = \frac{3n_{\text{He}} + 5n_{H_2}}{n_{\text{He}} + n_{H_2}}$$

$$= \frac{3 \times 5 + 5 \times 2}{(5 + 2)}$$

$$= 3.57 \text{ Ans.}$$

68. C

$$\gamma = \frac{C_p}{C_v} = \left[1 + \frac{2}{f} \right]$$

$$= \left[1 + \frac{2}{3.57} \right]$$

$$= 1.56 \text{ Ans.}$$

69. A

$$V/T = \text{const.} \quad P - \text{const.}$$

$$\Delta Q = nC_p \Delta T = n \frac{YR}{Y-1} \Delta T$$

$$\Delta w = nR \Delta R$$

$$\frac{\Delta Q}{\Delta W} = \frac{Y}{Y-1}$$

70. C

$$PV^r = \text{const}$$

$$V^r \frac{dP}{dV} = Y PV^{r-1} \frac{dV}{dV} = 0$$

$$\frac{dP}{dV} = \frac{-Y PV^{r-1}}{V^r} = \frac{-YP}{V}$$

$$= -1.4 \times \frac{.7 \times 10^5}{.0049}$$

$$= -2 \times 10^7$$

71. A

$$PV^m = \text{constant (K)}$$

$$P = \frac{K}{V^m} \Rightarrow \frac{P_1}{P_2} = \left(\frac{V_2}{V_1} \right)^m$$

$$P_2 = (2)^m P_1$$

$$Y_{\text{mono}} > Y_{\text{di}} > Y_{\text{tri}}$$

72. B

$$\Delta U = nC_v \Delta T$$

Given

$$6300 = \Delta U_i = nC_v (150)$$

$$\text{So, } \Delta U = \frac{6300}{150} \times 300$$

$$\Delta U = 12600$$

73. A

$$\Delta Q = \Delta U + \Delta W$$

$$= n \frac{f}{2} R \Delta T + n R \Delta T$$

$$= \left(1 + \frac{f}{2} \right) n R \Delta T$$

$$= \left(1 + \frac{6}{2} \right) n R \Delta T$$

$$= 4 [P \Delta V]$$

$$= 4 W = 100 J$$

74. A

$$\Delta W = \int_{V_1}^{V_2} P dV = \int_{V_1}^{V_2} K V dV \quad \because \frac{P}{V} = K$$

$$= \frac{K V_2^2 - K V_1^2}{2} = \frac{P_2 V_2 - P_1 V_1}{2}$$

$$\Rightarrow \Delta U = \frac{3}{2} R (2 T_0 - T_0) = \frac{3}{2} R T_0$$

$$\Delta Q = \Delta U + \Delta W$$

$$= 2 R T_0$$

75. D

$$\Delta Q = \Delta U + \Delta Q$$

$$2 C \Delta T = n \frac{f}{2} R \Delta T + P \Delta V$$

$$2 C \Delta T = 2 \times \frac{5}{2} R \Delta T + P \Delta V \quad \text{--- (1)}$$

$$\frac{P T^2}{V} = K$$

$$\text{or } \frac{T^3}{V^2} = \frac{K}{nR} \Rightarrow T^3 = \frac{K}{nR} V^2$$

$$\Rightarrow 3 T^2 dT = \frac{K}{nR} 2 V dV$$

$$\text{or } \frac{3 T^2}{2 V} dT = \frac{K}{nR} dV$$

$$\frac{3}{2} dT = \frac{P}{nR} dV \quad \text{--- (2)}$$

(1) and (2)

$$2 C \Delta T = 5 R \Delta T + n R \frac{3}{2} dT$$

$$2 C = 5 R + 3 R$$

$$2 C = 8 R$$

So, molar heat capacity $c = 4 R$ **76. B**

As suddenly compressed process is adiabatic

$$\therefore P_f = \frac{P_i}{2^r} \text{ (supposed halved)}$$

Now heat is released at constant volume.

$$P V = n R T$$

$$T \downarrow \quad \therefore P \downarrow$$

77. DThe process is adiabatic $\Delta Q = 0$ **78. C**

$$P V^Y = \text{Constant}$$

$$T V^{Y-1} = \text{Constant}$$

$$\frac{V_B}{V_C} = \left(\frac{T_1}{T_2} \right)^{Y-1} = \frac{V_A}{V_D}$$

79. C

Slope of adiabaic > isothermal

(A) (B)

80. C

Process is sudden so there is no time for heat transfer

$$\Delta U = -\Delta W = n C_v \Delta T$$

$$\Rightarrow \frac{\Delta U}{n} = C_v \Delta T$$

81. A(P) Isobaric $W = P \Delta V$

$$= PV$$

$$(Q) W = nRT \ln \frac{V_f}{V_i}$$

$$= PV \ln 2$$

(R) Adiabatic

$$W = \frac{PV(1-2^{1-y})}{y-1}$$

82. A,D

$$\Delta W = -\Delta U$$

$$\Rightarrow \Delta W + \Delta U = 0 = \Delta R$$

$$\Rightarrow \Delta Q = 0 \text{ (Adiabatic Process)}$$

83. D

$$PV^Y = K$$

$$\ln P + Y \ln V = \ln K$$

Differentiate

$$d(\ln P) + Y d(\ln V) = 0$$

$$\frac{d(\ln P)}{d(\ln V)} = -Y$$

$$Y_B > Y_A \Rightarrow \text{B is monoatomic}$$

Gas A is diatomic

84. B

$$\Delta U = n \frac{f}{2} R \Delta T$$

$$\text{Isobaric} \quad V_1 \rightarrow T_1 = \frac{P_1 V_1}{nR}$$

$$V_2 \rightarrow T_2 = \frac{P_1 (V_1/2)}{nR} = \frac{T_1}{2}$$

$$\Rightarrow \Delta U_P = \frac{nfR}{2} \left[\frac{T_1}{2} \right] \text{ ————— (1)}$$

$$\text{Isothermal} \quad \Delta U_T = 0 \text{ ————— (2)}$$

$$\text{Adiabatic} \quad PV^Y = K$$

$$TV^{y-1} = K$$

$$\frac{T_1}{T_2} = \frac{V_2^{y-1}}{V_1^{y-1}} = \frac{1}{2^{y-1}}$$

$$T_2 = 2^{y-1} T_1 > \frac{T_1}{2}$$

$$\Delta U_{\text{Adiabatic}} = n \frac{f}{2} R \left[2^{y-1} \right] \frac{T_1}{2}$$

$$\Delta U_{\text{adiabatic}} = \Delta U_P (2^{y-1}) \text{ ————— (3)}$$

85. D

For adiabatic

$$\frac{dP}{dV} = -Y \frac{P}{V}$$

$$\Rightarrow B = \frac{-dP}{(dV/V)} = YP = 1.4 \times 10^5 \text{ Pa}$$

86. A

Free Expansion

$$\text{So, } \left. \begin{array}{l} \Delta W = 0 \\ \Delta Q = 0 \end{array} \right\} \Rightarrow \Delta U = 0 \Rightarrow \Delta T = 0$$

$$\text{and } P_1 V_1 = P_2 (2 V_1)$$

$$P_2 = \frac{P_1}{2}$$

87. D

205

Ist Process

$$\Delta U_1 = \Delta Q_1 - \Delta W_1$$

$$= 16 - 20 = -4 \text{ KJ}$$

IInd Process

$$\Delta W_2 = \Delta Q_2 - \Delta U_2$$

$$\Delta U_1 = \Delta U_2 \quad (\because \Delta T = \text{same})$$

$$\text{So, } \Delta W_2 [9 - (-4)] = 13 \text{ KJ}$$

88. A

$$T_1^Y P_1^{1-Y} = T_2^Y P_2^{1-Y}$$

$$T_2 = T_1 \left(\frac{P_1}{P_2} \right)^{1-Y/Y}$$

$$= 300 \left(\frac{1}{4} \right)^{1-\frac{4/3}{4/3}}$$

$$= 300 \sqrt{2}$$